

EVALUATION OF TRAPPING MECHANISMS IN GEOLOGIC CO₂ SEQUESTRATION: CASE STUDY OF SACROC NORTHERN PLATFORM, A 35-YEAR CO₂ INJECTION SITE

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ABSTRACT. CO₂ trapping mechanisms in geologic sequestration are the specific processes that hold CO₂ underground in porous formations after it is injected. The main trapping mechanisms of interest include (1) fundamental confinement of mobile CO₂ phase under low-permeability caprocks, or stratigraphic trapping, (2) conversion of CO₂ to mineral precipitates, or mineral trapping, (3) dissolution in *in situ* fluid, or solubility trapping, and (4) trapping by surface tension (capillary force) and, correspondingly, remaining in porous media as an immobile CO₂ phase, or residual CO₂ trapping. The purpose of this work is to evaluate and quantify the competing roles of these different trapping mechanisms, including the relative amounts of storage by each. For the sake of providing a realistic appraisal, we conducted our analyses on a case study site, the SACROC Unit in the Permian basin of western Texas. CO₂ has been injected in the subsurface at the SACROC Unit for more than 35 years for the purpose of enhanced oil recovery. Our analysis of the SACROC production and injection history data suggests that about 93 million metric tons of CO₂ were injected and about 38 million metric tons were produced from 1972 to 2005. As a result, a simple mass-balance suggests that the SACROC Unit has accumulated approximately 55 million metric tons of CO₂.

Our study specifically focuses on the northern platform area of the SACROC Unit where about 7 million metric tons of CO₂ is stored. In the model describing the SACROC northern platform, porosity distributions were defined from extensive analyses of both 3-D seismic surveys and calibrated well logging data from 368 locations. Permeability distributions were estimated from determined porosity fields using a rock-fabric classification approach. The developed 3-D geocellular model representing the SACROC northern platform consists of over 9.4 million elements that characterize detailed 3-D heterogeneous reservoir geology. To facilitate simulation using conventional personal computers, we upscaled the 9.4 million elements model using a “renormalization” technique to reduce it to 15,470 elements. Analysis of groundwater chemistry from both the oil production formations (Cisco and Canyon Groups) and the formation above the sealing caprock suggests that the Wolfcamp Shale Formation performs well as a caprock at the SACROC Unit. However, results of geochemical mixing models also suggest that a small amount of shallow groundwater may be contaminated by reservoir brine possibly due to: (1) downward recharge of recycled reservoir brine from brine pits at the surface, or (2) upward leakage of CO₂-saturated reservoir brine through the Wolfcamp Shale Formation.

Using the upscaled 3-D geocellular model with detailed fluid injection/production history data and a vast amount of field data, we developed two separate models to evaluate competing CO₂ trapping mechanisms at the SACROC northern platform. The first model simulated CO₂ trapping mechanisms in a reservoir saturated with brine only. The second model simulated CO₂ trapping mechanisms in a reservoir saturated with both brine and oil. CO₂ trapping mechanisms in the brine-only model show distinctive stages accompanying injection and post-injection periods. In the 30-year

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injection period from 1972 to 2002, the amount of mobile CO₂ increased to 5.0 million metric tons without increasing immobile CO₂, and the mass of solubility-trapped CO₂ sharply rose to 1.7 million metric tons. After CO₂ injection ceased, the amount of mobile CO₂ dramatically decreased and the amount of immobile CO₂ increased. Relatively small amounts of mineral precipitation (less than 0.2 million metric tons of CO₂ equivalent) occurred after 200 years. In the brine-plus-oil model, dissolution of CO₂ in oil (oil-solubility trapping) and mobile CO₂ dominated during the entire simulation period. While supercritical-phase CO₂ is mobile near the injection wells due to the high CO₂ saturation, it behaves like residually trapped CO₂ because of the small density contrast between oil and CO₂. In summary, the brine-only model reflected dominance by residual CO₂ trapping over the long term, while CO₂ in the brine-plus-oil model was dominated by oil-solubility trapping.

Key words: Carbon dioxide, Geologic sequestration, CO₂ trapping mechanisms, Heterogeneity, Numerical Simulation, SACROC Unit.

INTRODUCTION

Over the past decade, the international scientific and engineering communities investigated the feasibility of long-term geologic sequestration of CO₂ in deep saline formations as a means of reducing atmospheric CO₂ levels (IEA, 2001; Gale, 2004; Orr, 2004; Thomas and Benson, 2005; Holloway, 2005; IPCC, 2005). Fundamental science questions considered and evaluated previously include:

1. **The physico-chemical properties of CO₂, brine, and CO₂-brine for predicting multiphase transport and solubility trapping** (Spycher and others, 2003; Duan and Sun, 2003; Bando and others, 2004; Portier and Rochelle, 2005; Spycher and Pruess, 2005; Dubessy and others, 2005; Duan and others, 2006, 2008; Fuller and others, 2006; Hu and others, 2007; Fleury and Deschamps, 2008; McPherson and others, 2008),
2. **Storage capacity estimation including appropriate storage site selection** (Bachu and Adams, 2003; NETL, 2005; Bradshaw and others, 2007; Bachu and others, 2007; Dilmore and others, 2008; Litynski and others, 2008; Núñez-López and others, 2008; Kopp and others, 2009),
3. **Spatiotemporal trapping mechanisms including hydrodynamic, residual, solubility, and mineral trappings** (Ennis-King and Paterson, 2005, 2007; Doughty and Pruess, 2004; Xu and others, 2004, 2005; Hellevang and others, 2005; Knauss and others, 2005; White and others, 2005; van der Meer and van Wees, 2006; Zerai and others, 2006; Farajzadeh and others, 2007; Ide and others, 2007; Parry and others, 2007; Flett and others, 2007; Audigane and others, 2007; Suekane and others, 2008; Zhou and others, 2008; Qi and others, 2009; Zhang and others, 2009),
4. **Caprock integrity** (Gaus and others, 2005; Chiquet and others, 2007; Gherardi and others, 2007; Plug and Bruining, 2007; Busch and others, 2008; Lu and others, 2009),
5. **Monitoring and verification including plume migration and groundwater impact** (Klusman, 2003; Emberley and others, 2004; Lewicki and others, 2005; Winthaegen and others, 2005; Gasperikova and Hoversten, 2006; Saripalli and others, 2006; Wells and others, 2007; Newell and others, 2008),
6. **Potential of CO₂ release from geologic storage sites** (Altevogt and Celia, 2004; Nordbotten and others, 2005; Pruess, 2005, 2008; Barlet-Gouédard and others, 2006; Oldenburg and Lewicki, 2006; Watson and Bachu, 2007; Cortis and others, 2008).

While these studies have successfully addressed most aspects of these questions, effective prediction of spatiotemporal CO₂ trapping mechanisms (mobile CO₂, residual CO₂, dissolved CO₂, and mineral) is still a challenging problem because it is

greatly affected by variability of subsurface conditions (pressure, temperature, and salinity), fluid properties (density, viscosity, solubility), and rock properties (porosity, permeability, and geochemical reactivity of minerals). Doughty and Pruess (2004) attempted to predict solubility trapping using a three-dimensional heterogeneous model of the fluvial/deltaic Frio Formation. They performed a numerical simulation to estimate CO₂ solubility trapping and storage capacity. Although their results showed strong interplay between geological heterogeneity and buoyancy-driven CO₂ flow, their model neglected both residual and mineral trapping. Kumar and others (2005) simulated the temporal variation of CO₂ trapping mechanisms in generalized three-dimensional, log-normally distributed permeability fields. They concluded that the relative degree of residual CO₂ trapping could be significantly greater than both solubility and mineral trapping mechanisms. Since residual CO₂ trapping is regarded as a most-effective trapping mechanism during the short term (hundreds of years), several studies specifically focused on investigating various aspects (for example, hysteresis, injection rate, water-alternating gas, and heterogeneity) to improve residual CO₂ trapping (Juanes and others, 2006; Ide and others, 2007; Flett and others, 2007; Doughty, 2007; Qi and others, 2009; Han and others, 2010a). Likewise, studies of mineral trapping include Xu and others (2004, 2005), Gaus and others (2005), White and others (2005), Zerai and others (2006), Audigane and others (2007), and Zhang and others (2009). Several different simulators were used in these studies, including TOUGHREACT, EQ3/6, CMG's GEM-GHG, ChemTOUGH2, PHREEQC, and Geochemist's Workbench (Wolery and Daveler, 1992; White, 1995; Bethke, 1996; Parkhurst and Appelo, 1999; Nghiem and others, 2004; Xu and others, 2006).

Despite the great deal of research on CO₂ trapping mechanisms, previous attempts to predict CO₂ trapping mechanisms appear to be hampered by several limitations:

- (1) Most previous models did not explicitly couple all CO₂ trapping mechanisms simultaneously. Rather, model simulations were focused on predicting one or two specific mechanisms.
- (2) Most previous models simplified their dimensions into either one or two, and neglected effects of heterogeneity.
- (3) Although some of the models used a three-dimensional grid, either spatial heterogeneity or the CO₂ injection data measured from the field were disregarded or not available.

A primary purpose of this research was to provide a detailed analysis of spatiotemporal CO₂ trapping mechanisms. We focused our analysis on a case study of the Scurry Area Canyon Reef Operations Committee (SACROC) Unit, a site with an abundance of actual CO₂ injection and production data; over 93 million metric tons of CO₂ were injected for the purpose of enhanced oil recovery since 1972 (Raines and others, 2001). We selected this site because vast amounts of data are available including (1) fluid injection/production history data since 1948, (2) water chemistry data of both reservoir brine and shallow groundwater, and (3) a 3-D high-resolution geocellular model that includes detailed characterization of reservoir structure and heterogeneity. The 3-D geocellular model employed in this study was developed using high-resolution geologic data (core data, well-logging data, sedimentologic and stratigraphic interpretation) and geophysical data (seismic attributes and rock physics data).

CO₂ INJECTION SITE: SACROC UNIT, TEXAS

Geologic Descriptions

The SACROC Unit is located in the southeastern segment of the Horseshoe Atoll within the Midland basin, western Texas (figs. 1A and B). Within the Horseshoe Atoll, the SACROC Unit comprises an area of 356 km² with an approximate north-south

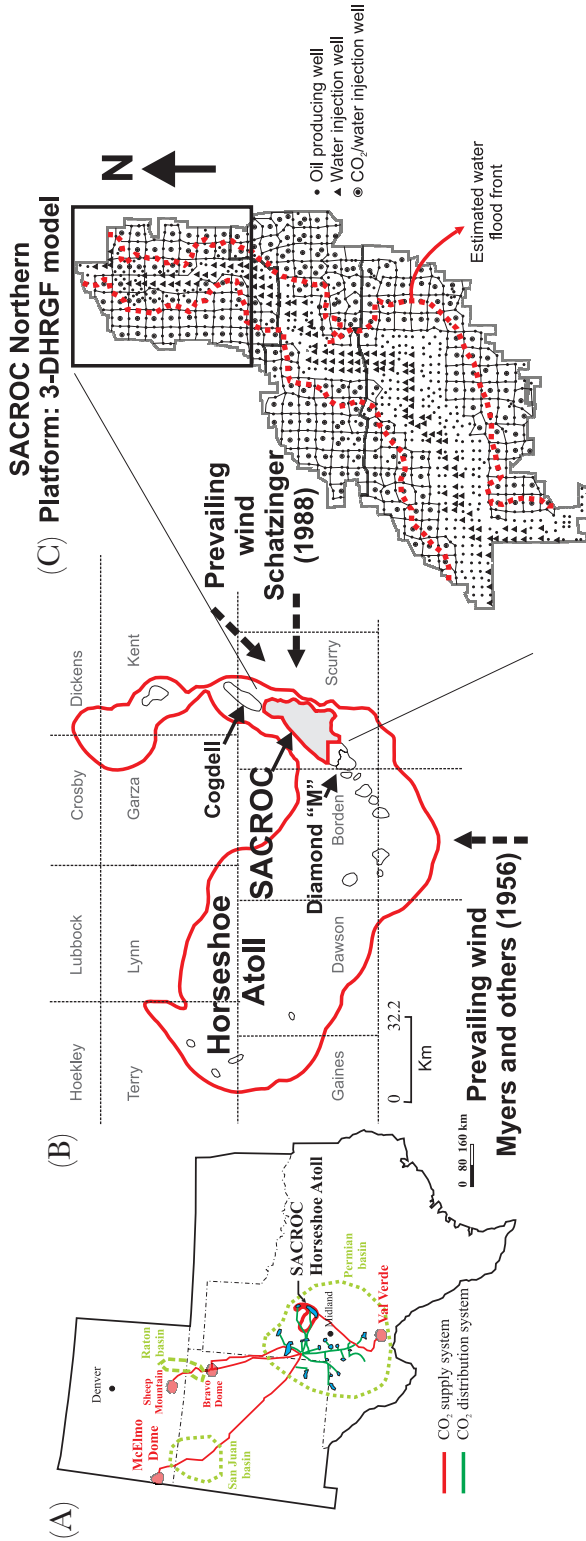


Fig. 1. (A) SACROC Unit at the Horseshoe Atoll in western Texas and CO₂ supply system from natural CO₂ reservoirs, (B) Magnified map of the SACROC Unit within the Horseshoe Atoll with indication of paleo-wind direction, (C) Well locations of SACROC Unit with the estimated water-flooding fronts at the end of water-flooding period in 1973 (Kane, 1979).

length of 40 km and an east-west length of 3 to 15 km (Vest, 1970). Geologically, the SACROC Unit is composed of massive amounts of bedded bioclastic limestone and thin shale beds representing the Strawn, Canyon, and Cisco Groups of the Pennsylvanian (Vest, 1970; Raines and others, 2001). The Wolfcamp Shale Formation of the lower Permian provides a low permeability caprock above the Pennsylvanian Cisco and Canyon Groups in the SACROC Unit. In detail, the Cisco and Canyon Groups are mostly composed of limestone with minor amounts of anhydrite. Sand, chert, and shale are present locally. Recently, Carey and others (2007) analyzed core samples from wells 49-5 and 49-6 in the SACROC Unit and indicated that the limestone was mostly calcite with minor ankerite, quartz, and thin clay lenses.

Previously, many petroleum geologists studied the SACROC Unit with respect to facies, depositional environment, and petrography (Bergenback and Terriere, 1953; Myers and others, 1956; Stafford, 1957; Stewart, ms, 1957; Burnside, 1959; Vest, 1970; Schatzinger, 1988; Reid and Reid, 1991; Walker and others, 1991; Raines and others, 2001). Several investigators have attempted to identify the depositional environments from the present distribution of carbonate lithofacies in this area. Their goal was to deduce the spatial locations of the high porosity zones to improve oil production by understating the depositional environment. Initially, Bergenback and Terriere (1953) inferred depositional environments from the distribution of carbonate lithofacies such as calcilutite (calcite mud) and oolitic limestone, which were respectively deposited in environments with calm water and strong currents. Myers and others (1956) discussed the possible theories of atoll growth and concluded that the “winds and currents” theory by Fairbridge (1950) accounted for the shape of the Horseshoe Atoll. Their research deduces conclusions that the direction of prevailing wind and currents was from south to north (fig. 1B). Later, Schatzinger (1988) recognized the spatial variation of oolites, which evidently decrease from north (Cogdell field) to south (Diamond M field), in the eastern portions of the Horseshoe Atoll and inferred that sedimentation was influenced by east-northeast prevailing winds (fig. 1B). Walker and others (1991) tried to identify the distribution of carbonate species and accretion of the Horseshoe Atoll by placing it in its paleolatitude and paleogeographic orientation (fig. 2). According to their research, the carbonate platform was on the equator in the early Strawn (312 Ma). From early Strawn (312 Ma) to middle Canyon (306 Ma), the relative motion of the carbonate platform was 63 degrees northeast and the platform accumulated at 2 degrees north. From early Cisco (298 Ma) to Wolfcampian (280 Ma), the direction of movement changed to 24 degrees northeast. As a result, the platform moved from 2 to 4 degrees north. Finally, carbonate accumulation stopped during the Wolfcampian at 6 degrees north due to the influx of fine-grained siliciclastics and dark shales (Walker and others, 1991). During its accumulation, prevailing winds from the northeast had a major impact on the distribution of carbonate facies, resulting in the percentage of oolitic carbonate being highest on the northeast-facing edges of the platform.

Along with an attempt to understand the spatial (aerial) distribution of carbonates in the SACROC Unit, previous researchers also investigated the variation of carbonates with depth and subsequently divided this Unit into Lower Canyon, Middle Canyon, Upper Canyon, and Cisco Groups through detailed analyses of cores, logging data, and biostratigraphy (fusulinid age) (fig. 3). Their analyses suggested that the Cisco Group, which was characterized as a highly heterogeneous group representing the dramatic changes in depositional environments, unconformably overlies the Canyon Group. The Upper Canyon is a highly porous zone, which includes erosional remnants resulting from a prolonged low sea level. The Middle/Lower Canyon Groups consist of high porosity layers separated by low porosity carbonate muds. More detailed

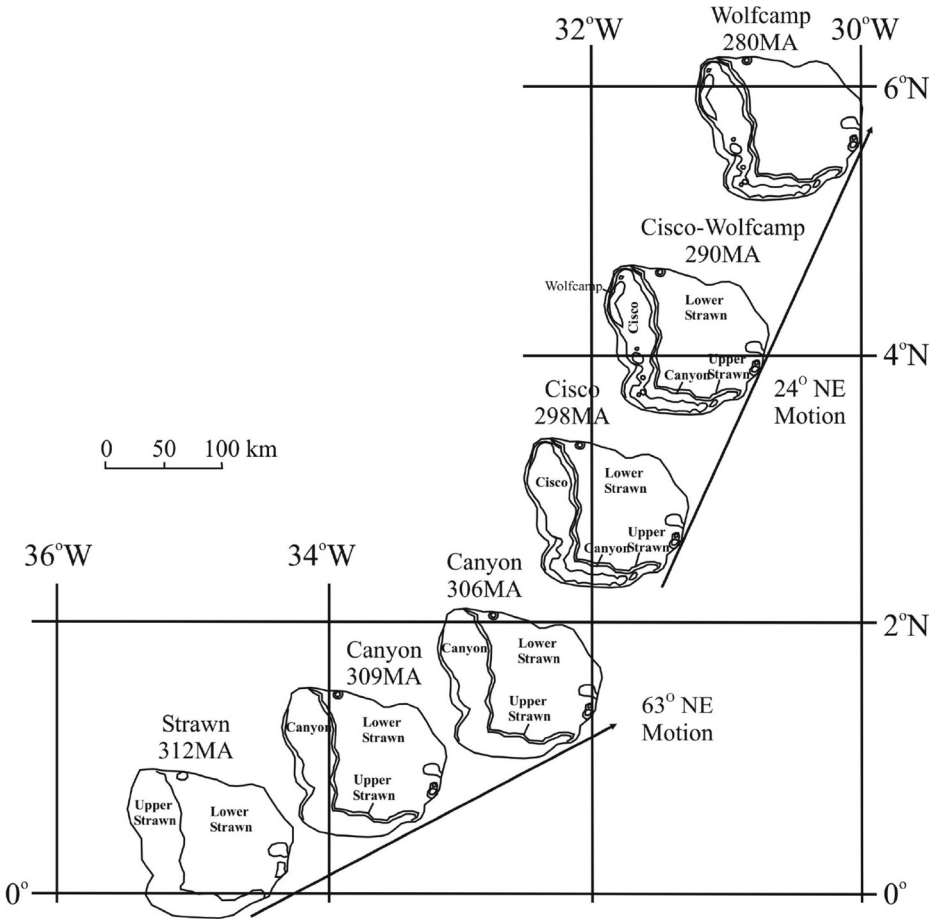


Fig. 2. The paleolatitude and paleogeographic location of the Horseshoe Atoll (Walker and others, 1991).

classification of the stratigraphy in the Cisco and Canyon Groups can be found in Reid and Reid (1991) and Hawkins and others (1996).

Changes in depositional environments show a wide variability of both porosity (0 to 30%) and permeability (0 to 1000 mD) in the Cisco and Canyon Groups (fig. 3). Bergenback and Terriere (1953) megascopically observed porosity distribution and reported values that ranged between approximately 0 to 20 percent. Similarly, Myers and others (1956) reported porosity values from 0 to 30 percent after core analysis. Both found that most porosity is developed during secondary diagenetic processes such as calcitization, dolomitization, and silicification. Burnside (1959) indicated that open fractures markedly influenced the permeability field. Other studies such as Vest (1970), Kane (1979), Langston and others (1988), Raines (2005), and Brnak and others (2006) provided average porosity and permeability, and the reader is referred to these studies for more detailed discussion.

Schatzinger (1988) estimated porosity from analysis of the depositional environment. In this study, the eastern part of the Horseshoe Atoll was spatially divided into three zones. The first zone included the Cogdell field and northern SACROC Unit

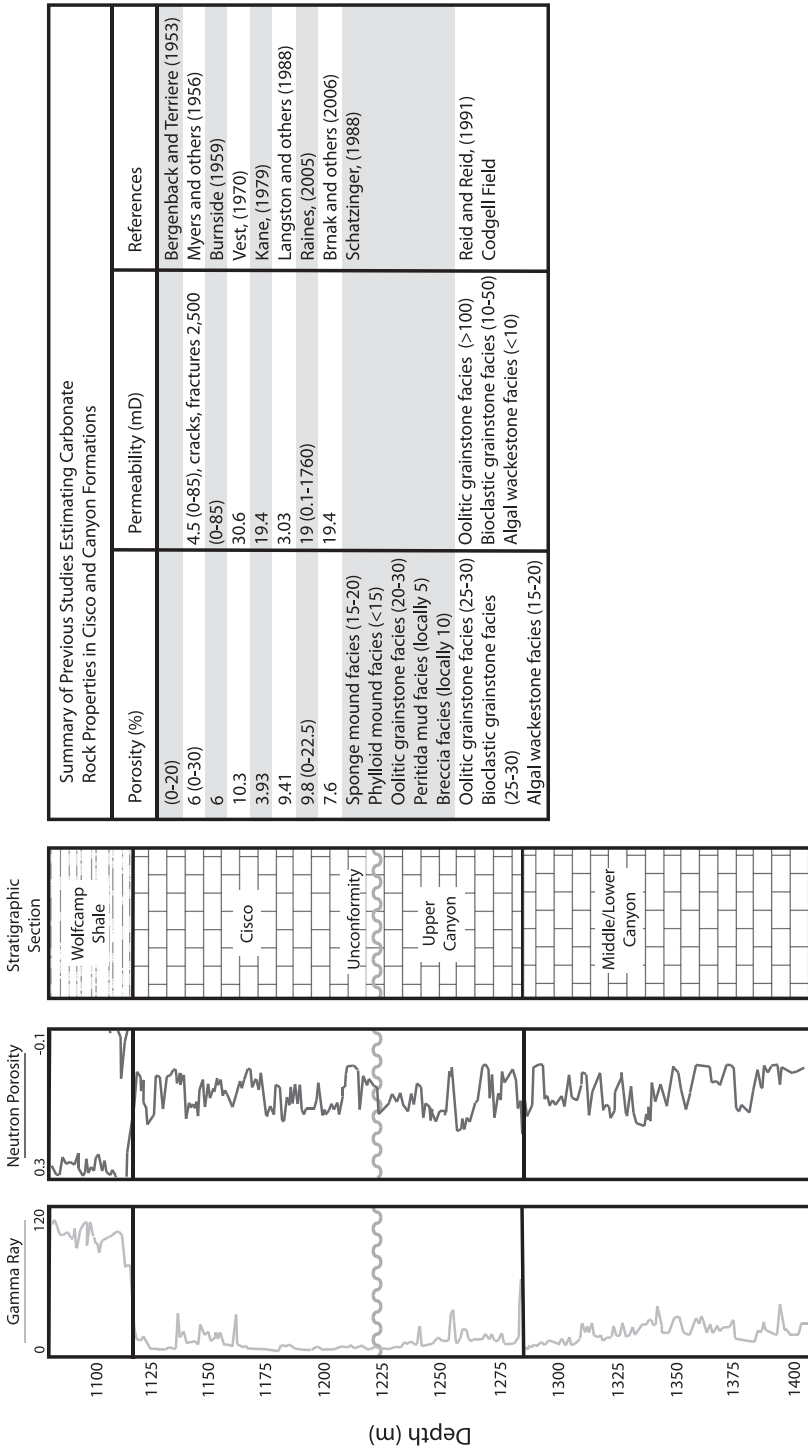


Fig. 3. Well logs representing the SACROC northern platform and summary of previous studies estimating carbonate rock properties in Cisco and Canyon Groups.

(fig. 1B), both reflecting turbulent environments with the deposition of basin-facing ooid shoals. The central and southern SACROC Unit shows intermediate turbulence conditions with the deposition of sponge-algal-bryozoan buildups. Finally, the Diamond M field and southern SACROC Unit reflect a low turbulence environment (fig. 1B). Research by Reid and Reid (1991) was more focused on the Cogdell field. In their work, the carbonate reef limestone was divided into nine zones after fusulinid age-dating and well logging correlations. Recently, there has been a similar effort to build stratigraphic frameworks and porosity distributions from the correlations of fusulinid biostratigraphy in the SACROC Unit (Hawkins and others, 1996). After examination of core and correlation with well logging, Hawkins and others (1996) found that porosity patterns were closely related to changes in depositional facies and suggested that the biostratigraphic distinction was significant in this field.

Injection and Production History

The SACROC Unit was discovered in 1948. The estimated original oil in place (OOIP) was approximated at 2.73 billion Stock Tank Barrels (STB) (Dicharry and others, 1973). From 1948 to 1951, over 1200 production wells were drilled in this Unit (Bayat and others, 1996). During this period, oil was produced by the solution gas drive mechanism resulting in reduction of the original reservoir pressure (3122 psi = 21.53 MPa) by over 50 percent (1560 psi = 11.38 MPa) for only 5 percent of OOIP production (Dicharry and others, 1973; Brummett and others, 1976).

To improve oil production and prevent crippling pressure loss, one of the largest pressure maintenance projects in the United States was started in 1954 (fig. 4). Fifty three water wells initiated water injection at a rate of approximately 21,000 m³ per day along the crest of the SACROC Unit (Allen and LaRue, 1957; Allen and Thomas, 1959; Dixon and Newton, 1965; Dicharry and others, 1973; Brummett and others, 1976; Bayat and others, 1996). The locations of water injection wells are shown in figure 1C. Before water injection began, only 1 percent of the reservoir was above the bubblepoint pressure (12.45 MPa). After 17 years (until 1971) of water injection, 77 percent of this Unit became above the bubblepoint pressure. The estimated waterflooding front at the end of waterflooding period in 1973 is shown in figure 1C. However, despite the high sweep efficiency of the water injection, approximately 1.2 billion STB of oil still remained in this Unit at the end of the water injection period. In addition, the repressurization plan eventually resulted in high reservoir pressure in the center of the SACROC Unit and low pressure towards the eastern and western margins. Because of the tremendous volume of oil still left in the reservoir after water injection, other enhanced oil recovery techniques were considered to improve oil recovery.

The SACROC field started with primary recovery, or the solution gas drive, then followed this with secondary recovery operations consisting of water-flooding. Based on engineering calculations, in 1972 the SACROC Unit operating committee decided that CO₂ injection would be the best tertiary oil recovery mechanism. The next major task was to find a CO₂ source near the SACROC Unit. The closest CO₂ sources were the Ellenburger hydrocarbon gas power plants in the Val Verde basin, about 220 miles (354 km) south of the SACROC Unit (fig. 1A). However, CO₂ from gas power plants were not ideal sources due to the lack of a consistent supply (gas power plants are subject to potential shutdowns due to their internal problems). Therefore, the SACROC operators switched CO₂ supply from gas power plants to McElmo Dome, a natural CO₂ reservoir in Colorado, in 1996 (Weeter and Halstead, 1982). The detailed characteristics including CO₂ accumulation in the CO₂ natural reservoir of McElmo Dome are discussed in Gerling (1983) and Allis and (2001). By changing the source of CO₂ from the gas power plants to a natural CO₂ reservoir, operations became more stable because of the continuous CO₂

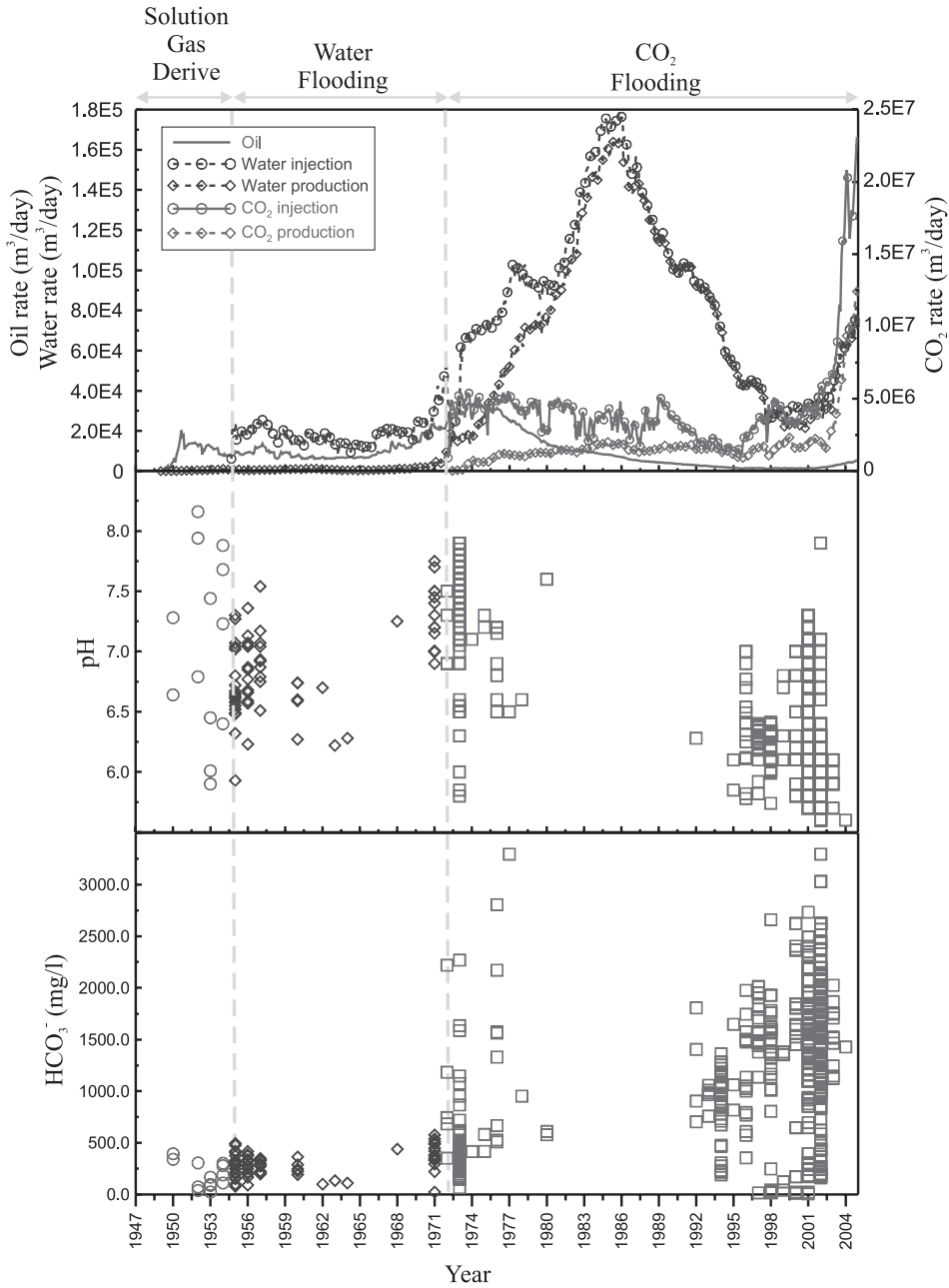


Fig. 4. Injection and production history of oil, water, and CO₂ (Raines, 2007) and corresponding evolution of pH and HCO₃⁻ in produced water from Cisco and Canyon Groups.

supply. In summary, about 93 million metric tons of CO₂ were injected and about 38 million metric tons were produced from 1972 to 2005 in this Unit. As a result, a simple mass-balance suggests that the site has accumulated about 55 million metric tons of CO₂ (Raines, 2005).

Effect of CO₂ Injection on Reservoir Brine Chemistry

Changes in reservoir brine chemistry due to injection of a massive amount of CO₂ have been observed in field-scale operations (Bowker and Shuler, 1991; Klusman, 2003; Emberley and others, 2004; Kharaka and others, 2006; Mito and others, 2008). These authors found that CO₂ dissolution typically results in the reservoir brine having a lower pH and higher HCO₃⁻ concentration. Subsequently, these reactions induce changes in reservoir rock properties. For this SACROC case study, we gathered and analyzed the brine chemistry data from the Cisco and Canyon Groups to investigate whether the similar alteration of reservoir brine chemistry, due to 35 years of CO₂ injection, occurred in the SACROC Unit. The brine chemistry data is a compilation of various analyses and reports from the Martin Water Laboratory, Unichem, the Texas Water Board, Permian Production Chemical, and the United States Geological Survey (Bowden, Kinder Morgan CO₂, personal communication, 2006). The statistical classification of these data sets, calculated for each period of differing oil-production mechanisms, is shown in table 1.

Statistics of the SACROC reservoir brine chemistry (table 1) show that mean concentration of Na⁺ and Cl⁻ were respectively 27,292 mg/L and 51,496 mg/L during the solution gas period (1948-1952) and their concentration decreased to 24,750 mg/L and 46,263 mg/L throughout the waterflooding period (1953-1971). This dilution of reservoir brine is the result of relatively fresh water being injected and recycled during the waterflooding period. Similarly, the dilution of reservoir brine during the waterflooding period has been observed in another oilfield, the Rangely Field, Colorado. Brine salinity before waterflooding was approximately 100,000 ppm in Rangely Field but it decreased to 33,000 ppm at the end of waterflooding (Bowker and Shuler, 1991). After the initiation of CO₂ flooding in the SACROC Unit (1972-2004), it was expected that increases of Na⁺, Cl⁻, and other species' concentrations would occur, similar to the observations made in Rangely Field, Colorado by Klusman (2003). However, mean values of Na⁺, Ca²⁺, Cl⁻, and SO₄²⁻ concentrations kept decreasing during the CO₂ flooding period in the SACROC Unit (table 1). We presume that this difference occurred because the SACROC operators performed waterflooding prior to CO₂ injection even during the CO₂ flooding period to increase reservoir pressure to minimum miscibility pressure and also employed Water-Alternating-Gas (WAG) processes. Therefore, huge amounts of water were injected and recycled even in the CO₂ flooding period (fig. 4), and caused the continued dilution of reservoir brine. In addition, the CO₂ injection formation in Rangely Field, Colorado, is sandstone but it is limestone in the SACROC Unit. Therefore, the potential chemistry changes between these two reservoirs due to CO₂ injection are expected to be different.

Evolving patterns of both pH and HCO₃⁻ concentrations shown in figure 4 are similar to the observations from other field-scale operations (Klusman, 2003; Emberley and others, 2004; Kharaka and others, 2006; Mito and others, 2008). The pH becomes lower and the HCO₃⁻ concentration increases from the waterflooding period until the CO₂ flooding period. Especially, in the SACROC Unit, where the decrease in pH during CO₂ flooding was small (6.88 to 6.43 shown in table 1) compared with the pH decrease in the Rangely field (6.69 to 5.50; Kluseman, 2003) and Frio field (6.7 to 5.5; Kharaka and others, 2006) where the formation rocks are sandstone. This result suggests that carbonate rock, which is the major rock in the SACROC Unit, buffered the drop in pH. The dramatic increase of HCO₃⁻ (306.90 to 1313.69 mg/L) is possibly caused by both the injected CO₂ being dissolved in the brine solution and the dissolution of calcite (CaCO₃) and dolomite (CaMg(CO₃)₂). Notably, the concentration of Mg²⁺ in the reservoir brine increased (917.90 to 1,305.01 mg/L) during the CO₂ flooding period, suggesting that CO₂ injection possibly caused the dissolution of Mg-bearing minerals such as dolomite (CaMg(CO₃)₂) and Magnesite (MgCO₃).

TABLE 1

Statistics of water chemistry analyses and chemical modeling of reservoir fluids in Cisco and Canyon Groups during each oil production mechanism

Oil Production Mechanisms		Solution gas	Water flooding	CO ₂ flooding
Period (Year)		1948-1952	1953-1971	1972-2004
Number of samples		13	69	758
Reservoir pressure (MPa)		21.50	11.38	16.55
Reservoir temperature (°C)		54.50	54.50	54.50
pH	Mean	7.06	6.88	6.43
	Std.	0.75	0.37	0.60
Na ⁺ (mg/L)	Mean	27,292.00	24,750.72	24,248.52
	Std.	11,011.07	11,026.97	9,192.98
Ca ²⁺ (mg/L)	Mean	4,238.15	3,613.78	2,675.24
	Std.	2,256.80	2,065.09	1,644.09
Mg ²⁺ (mg/L)	Mean	959.92	917.90	1,305.01
	Std.	444.99	464.05	833.68
Cl ⁻ (mg/L)	Mean	51,496.46	46,263.46	44,587.90
	Std.	21,838.31	21,068.02	16,665.64
HCO ₃ ⁻ (mg/L)	Mean	185.15	306.90	1313.69
	Std.	125.06	112.78	675.52
SO ₄ ²⁻ (mg/L)	Mean	1,675.31	1,050.61	782.80
	Std.	755.17	697.64	679.30
CO ₂ fugacity (MPa)	Mean	3.64* (0.0169)	3.35** (0.0294)	67.68*** (0.4089)
	Std.	3.77*	1.72**	54.36***
SI of calcite (CaCO ₃)	Mean	0.68	0.80	0.62
	Std.	0.92	0.47	0.78
SI of dolomite (CaMg(CO ₃) ₂)	Mean	2.28	2.55	2.44
	Std.	1.81	0.95	1.51
SI of Magnesite (Mg(CO ₃))	Mean	0.13	0.28	0.35
	Std.	0.89	0.49	0.80
SI of anhydrite (CaSO ₄)	Mean	-0.43	-0.69	-1.00
	Std.	0.26	0.26	0.46
SI of gypsum (CaSO ₄ ·H ₂ O)	Mean	-0.57	-0.83	-1.14
	Std.	0.27	0.26	0.46

*, **, and *** is respectively calculated with reservoir pressure 21.5, 11.38, and 16.55 MPa because reservoir pressure varies historically (Dicharry and others, 1973; Brummett and others, 1976). Parentheses indicate the normalized CO₂ fugacity at 0.1 MPa. Reservoir temperature is from Langston and others (1988). SI represents the saturation index of mineral.

CO₂ fugacity can be an indicator as to whether injected CO₂ was dissolved in the reservoir brine, and the Saturation Indexes (SI) of minerals can provide key information associated with the degree of mineral saturation in the reservoir brine. Therefore, CO₂ fugacity and SI of representative carbonate and sulfate minerals are calculated with the B-dot activity coefficient model (Helgeson, 1969) using Geochemist's Workbench (GWB™) version 7.0 (Bethke, 1996). The statistics for the modeled CO₂ fugacity in table 1 show that the mean of modeled CO₂ fugacity is similar throughout the solution gas (3.64 MPa) and waterflooding (3.35 MPa) periods. However, the mean value of the modeled CO₂ fugacity significantly increased to 67.68 MPa during the CO₂ flooding period showing the evidence of CO₂ dissolution in reservoir brine. The

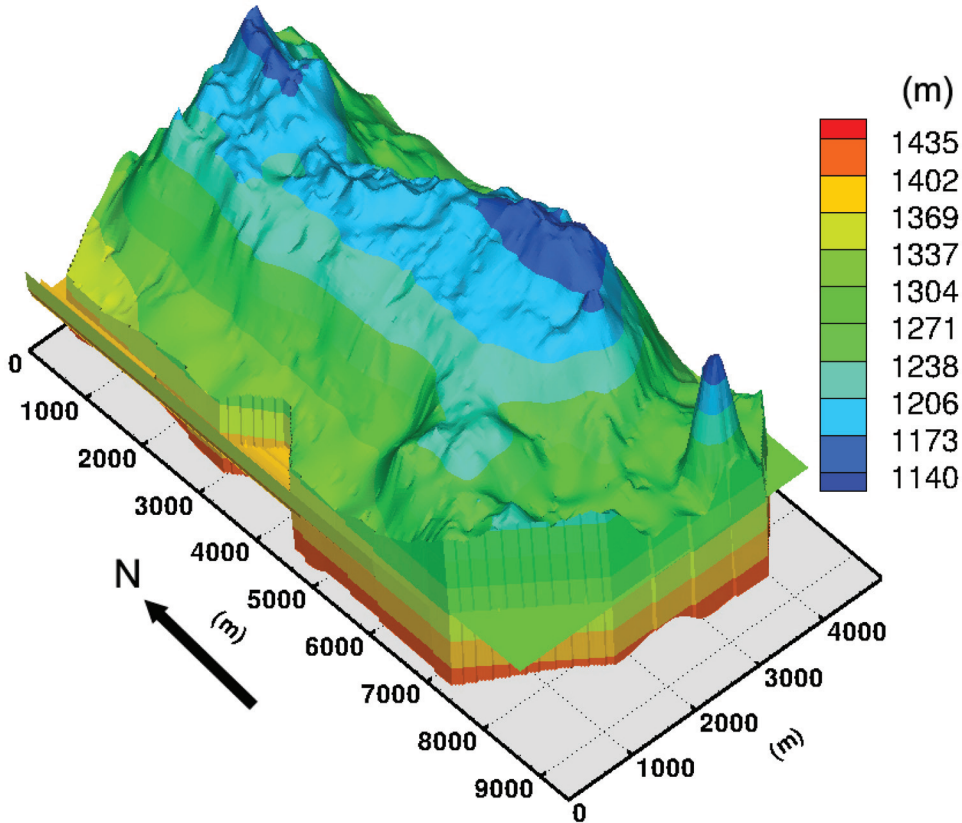


Fig. 5. Structure of 3-D geocellular model representing Cisco and Canyon Groups in the SACROC northern platform. Label (m) indicates the formation depth from the sea level.

modeled SI values suggested that the reservoir brine in the Cisco and Canyon Groups was oversaturated with carbonate minerals but it was undersaturated with anhydrite and gypsum during the entire oil production period (1948-2004). Although the chemistry of the dissolved species in the reservoir brine evolves during oil production periods (fig. 4 and table 1), the saturation states of minerals did not significantly vary, suggesting that chemical reactions between dissolved species are relatively faster than water-rock interaction. In addition, this analysis also suggests that 35 years is not enough time to predict definite changes of mineral saturation states.

DESCRIPTION OF 3-D, HIGH-RESOLUTION GEOCELLULAR MODEL IN SACROC NORTHERN PLATFORM AND UPSCALING

The 3-D geocellular model representing the Cisco and Canyon Groups in the SACROC northern platform is illustrated in figure 5. The approximate size of the model is 4,000 m wide and 10,000 m long. The top of the geocellular model shows the upper configuration of the Cisco Group, which is approximately 1200 m below sea level, and the bottom of the model shows the lower configuration of the Canyon Group, which is a depth of approximately 1400 m below sea level.

Figures 6A–D show the external and internal distributions of both porosity and permeability. In this model, porosity distributions were defined from both 3-dimensional seismic surveys and 368 well logging analyses. Subsequently, permeability

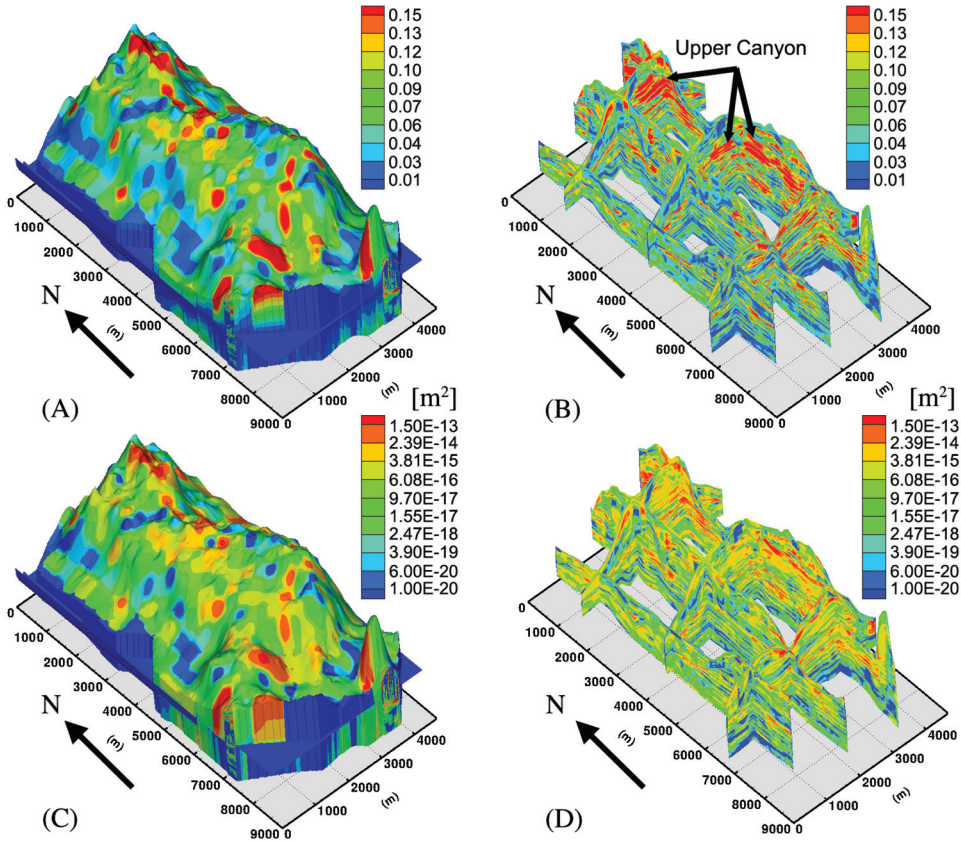


Fig. 6. Internal and external distributions of porosity and permeability in the 3-D geocellular model: (A) external distribution of porosity, (B) internal distribution of porosity, (C) external distribution of permeability (m²), and (D) internal distribution of permeability (m²).

distributions were calculated from seismically calibrated porosity distributions using empirical equations derived from rock fabric classification (Lucia and Kerans, 2004). The global transforming equation has been derived for carbonate rock as (Lucia, 1995, 1999; Jennings and Lucia, 2003):

$$\log(k) = (9.792 - 12.0838\log(\lambda)) + (8.6711 - 8.2965\log(\lambda))\log(\phi) \quad (1)$$

where, λ , k , and ϕ are, respectively, rock-fabric number, permeability, and interparticle porosity. Specifically, λ represents the specific class of carbonate rock based on petrophysical properties such as inter-particle porosity in tandem with geological descriptions of particle size and sorting. Lucia and Kerans (2004) applied this equation to estimate the permeability distribution in the SACROC northern platform. The detailed parameters of rock-fabric numbers in this model are described in table 2.

This 3-D geocellular model preserves the detailed heterogeneity variation of both porosity and permeability (figs. 6A-D). The model reveals that the Cisco and Canyon Groups typically lie within a “stacked system” of alternating high and low porosity layers (fig. 6B). The thick and high porous zone shown in figure 6B represents the Upper Canyon Group. The Cisco Group is located above the Upper Canyon Group, and the Middle/Lower Canyon Groups are below the Upper Canyon Group. Specifically, the

TABLE 2

Permeability estimation using porosity and rock-fabric number (Lucia and Kerans, 2004)

Formation	Sequence	Rock- fabric number (λ)	Transforming equations	
Cisco	1	Reduced major axis transformation	$k = 2.1625 \times 10^6 \times \phi^{3.8844}$	Highest portion of Cisco (Implication of karsting)
	2	1.7	$k = 1.031 \times 10^7 \times \phi^{6.7592}$	Late Cisco (wide variety of rock fabrics)
	3	1.9	$k = 2.69 \times 10^6 \times \phi^{6.3584}$	Early Cisco (Characterized by fusulinid/crinoidal/peloid grain dominated packstones, grainstones, and wackestones)
Canyon	1	2.5	$k = 97628 \times \phi^{5.3696}$	Early Canyon: (Characterized by moldic ooid grainstone, grain-dominated packstone, and mud-dominated fabrics)
	2	1.75	$k = 38520 \times \phi^{5.0923}$	Late Canyon: (Characterized by crinoidal/fusulinid/peloid, grain-dominated packstones, and mud-dominated fabrics having vuggy porosity)

Middle/Lower Canyon Groups consist of several layered high porosity zones separated by low-porosity carbonate mud.

The 3-D geocellular model describing the Cisco and Canyon Groups includes 9,450,623 ($149 \times 287 \times 221$) elements (figs. 5 and 6). Although the model provides a quantified characterization of the natural heterogeneity of both porosity and permeability distributions in the SACROC northern platform, the utilization of this model in describing CO₂ trapping mechanisms was hampered due to the large number of elements; only supercomputers capable of massively parallel computation can accommodate simulations of this model. For this reason, we elected to upscale the model to fewer elements. Such upscaling invariably results in a loss of heterogeneity resolution, but we tried to preserve as much of this heterogeneity as possible. The purpose of upscaling was two-fold: (1) about 9.4 million elements exceeded the memory capacity of our model simulators on a personal computer and (2) the original porosity and permeability data as estimated from geophysical data varied extremely from cell-to-cell, sometimes as much as several orders of magnitude in permeability. Upscaling smoothes these data through the averaging process and facilitates a more stable numerical solution, albeit with the loss of heterogeneity resolution.

In this study, porosity is upscaled by the volumetric averaging technique, and permeability (k) is upscaled with an algorithm developed through an equivalent resistor network model (King, 1989). The upscaling equation and conceptual diagram used in this work is shown in eq 2 and figure 7, respectively.

$$k_{eff} = \frac{4(k_1 + k_3)(k_2 + k_4)[k_2 k_4 (k_1 + k_3) + k_1 k_3 (k_2 + k_4)]}{[k_2 k_4 (k_1 + k_3) + k_1 k_3 (k_2 + k_4)][k_1 + k_2 + k_3 + k_4] + 3(k_1 + k_2)(k_3 + k_4)(k_1 + k_3)(k_2 + k_4)} \quad (2)$$

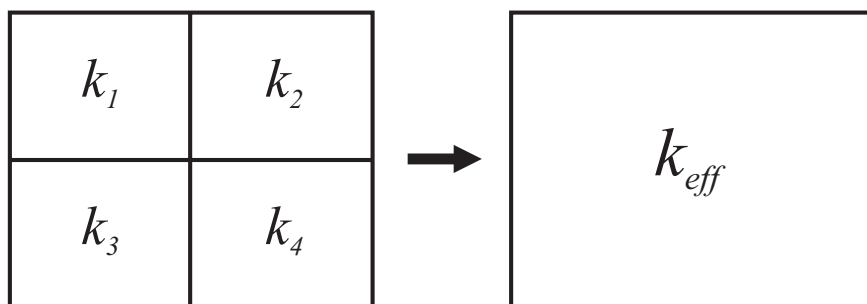


Fig. 7. Upscaled permeability using renormalization and the equivalent equation is shown in eq 2.

This technique is generally called “renormalization” because it successively upscales the symmetric grid-blocks using self-repetitive geometry until the final grid-block size is reached. Using this approach is fast and computationally cheap because it does not require solutions to the differential equations. In addition, it is not constrained by the number of grid-blocks. Because of these practical advantages, many researchers have studied and updated renormalization techniques (Hinrichsen and others, 1993; King, 1996; Gautier and Noetinger, 1997; Renard and others, 2000). Despite its many advantages, renormalization has several drawbacks. If there is a high contrast between neighboring permeability values, using this approach will underestimate the upscaled permeability value (King, 1989; Renard and de Marsily, 1997). In addition, this method has some limitations with respect to applicable boundary conditions (Malick, ms, 1995). Finally, renormalization is specially designed for orthogonal grids. Although our model satisfies several conditions to apply this renormalization technique, the grid is not completely orthogonal. The grid is orthogonal in both the x- and y-direction; however, the z-direction is irregular, which could induce some error in the resulting upscaled permeability. It is extremely difficult to quantify the error due to this non-orthogonality, although we estimate the accrued error to be less than the uncertainty associated with seismic and well logging data used to calibrate the model.

Sequential results of permeability distributions by renormalization are shown in figure 8. In addition, the detailed statistics of permeability values, the number of grid-blocks, and their sizes are shown in table 3. As the grid is upscaled, the size of grid-block becomes greater, and both the means (arithmetic, harmonic, and geometric) and standard deviation of the permeability become smaller. Decrease in the means of upscaled permeability suggests that low permeability values have a greater influence on the calculation of upscaled permeability values. Similarly, decrease in standard deviation of upscaled permeability suggests that permeability distribution from cell-to-cell becomes smoother. Finally, for the model development utilized for the simulation of CO₂ trapping mechanisms in the SACROC northern platform, we obtained the upscaled grid with 15,470 elements shown in figure 8D.

DETERMINATION OF BOUNDARY CONDITIONS: EVALUATION OF WOLFCAMP SHALE FORMATION
AS A SUITABLE SEAL

To evaluate the seal integrity of the Wolfcamp Shale Formation, we gathered and analyzed the available water chemistry data to determine the potential sealing effect of this formation. These chemical analyses do not provide definitive proof to whether or not CO₂ leaks through the Wolfcamp Shale Formation because the SACROC Unit comprises a huge area, 356 km² (fig. 1). Even the most detailed datasets will not cover

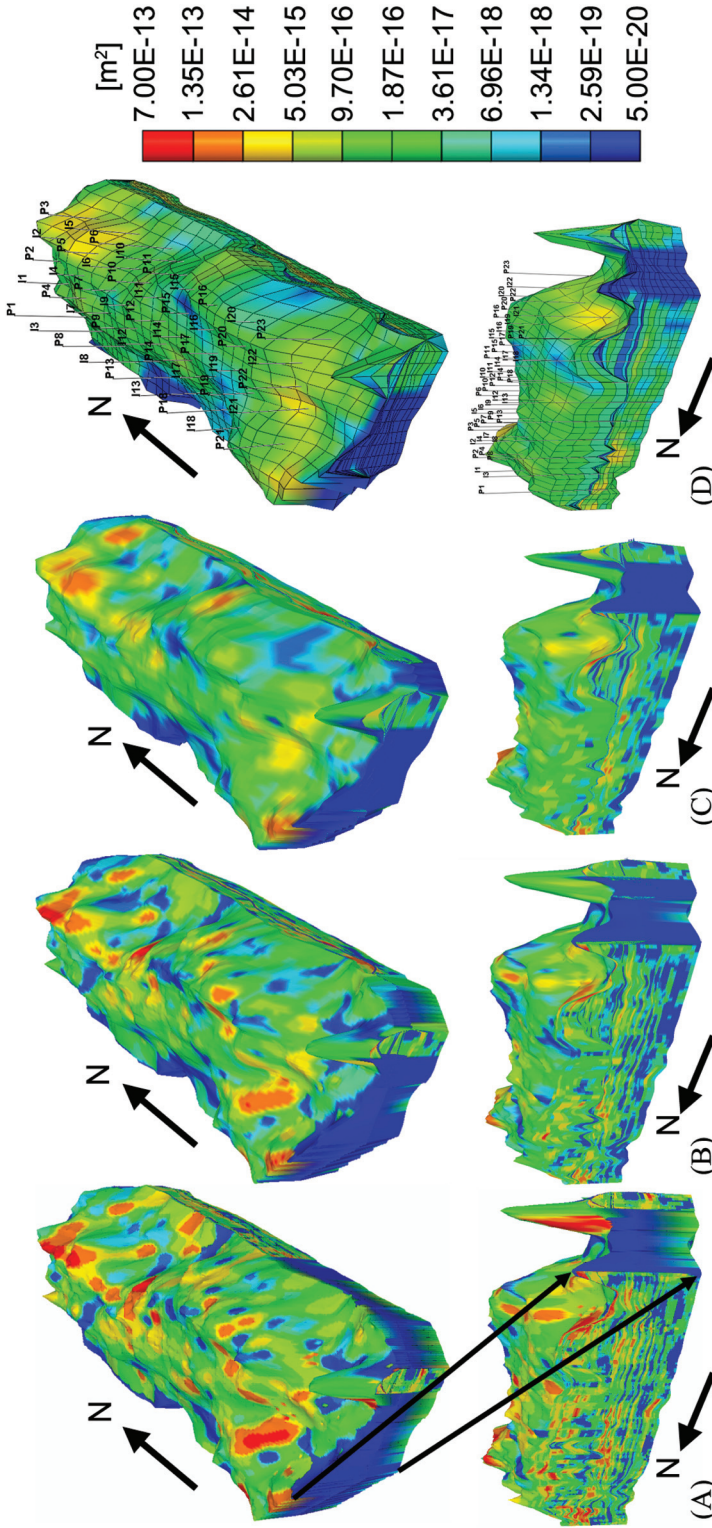


Fig. 8. Internal and external permeability distributions during each renormalization procedure. The detailed grid statistics are shown in table 2: (A) 149×287×221=9,450,623 elements, (B) 74×143×110=1,164,020 elements, (C) 36×71×54=139,908 elements, and (D) 17×35×26=15,470 elements.

TABLE 3

Detailed statistics of permeability, grid dimensions, and size of grids during the renormalization process

	Number of Grid			Total number of Grids	Grid size (m)			Permeability (m ²)			Std. dev.
	X	Y	Z		X	Y	Z	Arithmetic	Harmonic	Geometric	
1	149	287	221	9,450,623	30.54	30.46	vary	5.62E-15	8.75E-20	2.13E-18	4.20E-14
2	74	143	110	1,164,020	61.08	60.91	vary	3.58E-15	8.46E-20	1.58E-18	2.40E-14
3	36	71	54	139,968	122.16	121.83	vary	1.93E-15	8.21E-20	1.12E-18	1.38E-14
4	17	35	26	15,470	244.32	243.66	vary	5.10E-16	7.45E-20	5.76E-19	3.26E-15

the entire area of SACROC Unit. As such, the ultimate goal of these analyses is to evaluate the overall performance of the Wolfcamp Shale Formation and evaluate the likelihood that the Wolfcamp Shale Formation currently acts as a suitable seal in this area.

During the geologic time period, the Wolfcamp Shale Formation about 150 m thick was the caprock overlying the hydrocarbon in the Cisco and Canyon Groups (Vest, 1970; Raines and others, 2001). Although CO₂ has been injected during the last 35 years, previous researchers have not reported any indication of CO₂ leakage such as travertine deposits at the surface, changes of shallow groundwater chemistry, anomalous CO₂ gas concentration at the surface, or changes in surface vegetation over time. In addition, several scientific investigations supported the premise that the Wolfcamp Shale Formation might be a suitable seal within the SACROC Unit. For example, Carey and others (2007) measured vertical permeability of the Wolfcamp Shale Formation and suggested that it is low enough (<0.05 mD) to build a capillary barrier that hampers buoyancy-driven migration of CO₂. In addition, their mineralogical and isotopic (oxygen and carbon) analyses suggested that the carbonates in the Wolfcamp Shale Formation appear to be derived from primarily diagenetic processes, supporting that CO₂ is effectively trapped in the Cisco and Canyon Groups.

For this study, we gathered and analyzed the available water chemistry data to determine the potential sealing efficacy of the Wolfcamp Shale Formation. Detailed statistics of brine samples (840) gathered from the Cisco and Canyon Groups are shown in table 1, and those for shallow groundwater samples (170) gathered from the Dockum formation above the Wolfcamp Shale Formation are summarized in table 4. A Piper diagram analysis in Han (ms, 2008) illustrated that the chemistry of the shallow groundwater is distributed from Na-HCO₃ to Ca-HCO₃ while most of the brine is the Na-Cl type.

With a similar approach to analyzing reservoir brine as described in the previous section, “*Effect of CO₂ Injection on Reservoir Brine Chemistry*”, we calculated the CO₂ fugacity and saturation indexes (SI) of minerals from shallow groundwater. Interestingly, mean values of CO₂ fugacity from the shallow groundwater did not change from water flooding to CO₂ injection period (table 4), suggesting that CO₂ injection into the Cisco and Canyon Groups did not significantly impact the chemistry of the shallow groundwater above the Wolfcamp Shale formation. In addition, SI analysis suggests that shallow groundwater is oversaturated with respect to calcite and dolomite, but the degree of oversaturation in the shallow groundwater is smaller than that in the reservoir brine of Cisco and Canyon Groups.

We hypothesized that the concentrations of reservoir brine in the Cisco and Canyon Groups and shallow groundwater above the Wolfcamp Shale Formation would

TABLE 4

Statistics of water chemistry analyses and chemical modeling of shallow groundwater above Wolfcamp Shale Formation (Dockum aquifer) during each oil production mechanism

Oil Production Mechanisms		Solution gas	Waterflooding	CO ₂ flooding
Period (Year)		1948-1952	1953-1971	1972-2004
Number of samples		No sample	48	122
Temperature (°C)	Mean		20.85	21.03
	Std.		0.67	1.15
pH	Mean		7.48	7.63
	Std.		0.47	0.68
Na ⁺ (mg/L)	Mean		278.98	349.26
	Std.		383.12	1009.94
Ca ²⁺ (mg/L)	Mean		104.18	125.67
	Std.		130.81	126.47
Mg ²⁺ (mg/L)	Mean		46.03	40.92
	Std.		65.08	41.86
Cl ⁻ (mg/L)	Mean		336.13	484.66
	Std.		631.31	1552.49
HCO ₃ ⁻ (mg/L)	Mean		323.27	304.09
	Std.		105.38	81.21
SO ₄ ²⁻ (mg/L)	Mean		292.16	284.57
	Std.		461.91	421.18
SiO ₂ (aq) (mg/L)	Mean		22.15	25.17
	Std.		11.26	10.53
CO ₂ fugacity (MPa)	Mean		0.009	0.009
	Std.		0.007	0.010
SI of calcite (CaCO ₃)	Mean		0.08	0.45
	Std.		0.44	0.49
SI of dolomite (CaMg(CO ₃) ₂)	Mean		0.91	1.53
	Std.		0.87	1.00
SI of Magnesite (Mg(CO ₃))	Mean		-0.83	-0.58
	Std.		0.46	0.53
SI of anhydrite (CaSO ₄)	Mean		-2.24	-2.03
	Std.		0.81	0.71
SI of gypsum (CaSO ₄ ·H ₂ O)	Mean		-2.01	-1.80
	Std.		0.81	0.71

CO₂ fugacity is calculated with a pressure of 0.1 MPa. SI represents the saturation index of mineral.

show the evidence of a mixing effect if CO₂-saturated reservoir brine leaked through highly permeable conduits such as faults or fractures in the Wolfcamp Shale Formation. The flow system in the Cisco and Canyon Groups are advection-dominant due to a significant alteration of pressure by injection and production activities. Such conditions may accelerate the migration of reservoir brine through highly permeable conduits with the result that CO₂-saturated reservoir brine may make its way to the above shallow groundwater zone.

To evaluate the potential chemical signatures of such mixing effects, we simulated equilibrium mixing with mean values of dissolved species from both reservoir brine and shallow groundwater collected during CO₂ flooding periods (tables 1 and 4),

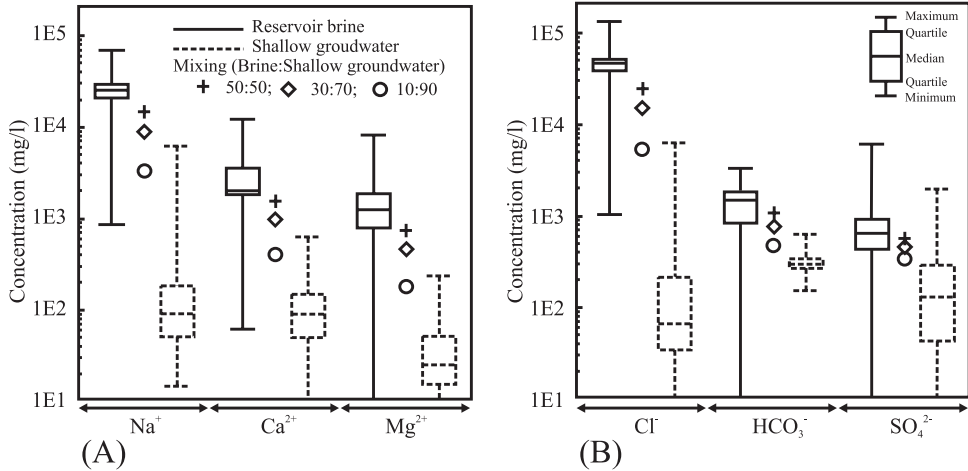


Fig. 9. Box-and-whisker diagram showing the range of brine and shallow groundwater, and results of equilibrium mixing model simulated after varying the volume of reservoir brine (10, 30, and 50%).

using PHREEQC version 2.15.0 with thermodynamic data known as phreeqc.dat (Parkhurst and Appelo, 1999). Three sets of mixing models were simulated after varying the volume of reservoir brine (10, 30, and 50%). The simulation results are plotted in the Box-Whisker plot between concentrations of individual species in the reservoir brine and shallow groundwater (fig. 9). The plot shows that concentrations of dissolved species between reservoir brine and shallow groundwater are typically different and generally provide no distinct indication of communication. However, results of the equilibrium mixing model show that a few shallow groundwater samples potentially show the mixing effect with reservoir brine. Results of 10 percent-brine mixing simulations (circle in fig. 9) are plotted within the range of both brine and shallow groundwater. In detail, less than 5 percent of shallow groundwater samples have a concentration greater than the modeled concentration of the 10 percent-brine mixing model. This analysis suggests that a few shallow groundwater samples might be locally contaminated with reservoir brine. However, it is difficult to conclude that the contamination of shallow groundwater is mainly due to the leakage of CO₂-saturated reservoir brine through the Wolfcamp Shale Formation. In the SACROC Unit, there exist many brine pits on the surface used to store recycled reservoir brine. Therefore, it is possible that this stored reservoir brine on the surface could recharge downward into the shallow groundwater zones and induce the contamination of shallow groundwater.

Based on the analysis of brine and shallow groundwater chemistry, we concluded that the Wolfcamp Shale Formation generally acts as a suitable seal in the SACROC Unit. Previous results of CO₂ fugacity calculation showed that there was no significant increase of modeled CO₂ fugacity in shallow groundwater (table 4) although the modeled CO₂ fugacity of reservoir brine in the Cisco and Canyon Groups significantly increased during the CO₂ flooding period. In addition, the equilibrium mixing model shows that only less than 5 percent of shallow groundwater samples displays the evidence of mixing effects with reservoir brine. Even then, it is also possible that this mixing is due to the downward recharge of recycled brine from brine pits at the surface during enhanced oil recovery.

SOURCES AND SINKS: ACTUAL CO₂ INJECTION AND PRODUCTION HISTORIES

We analyzed CO₂ injection and production histories provided by Kinder Morgan CO₂ Inc. in the SACROC northern platform. According to these records,

97 wells were used as CO₂ injectors at the SACROC northern platform from 1972 to 2002. Among them, 51 wells were actively used to inject about 13 million metric tons of CO₂ (13,048,845,748 kg) into Cisco and Canyon Groups. Another 219 wells were used as CO₂ producers during the same period. Among them, 124 wells were actively used to produce about 6 million metric tons of CO₂ (6,104,258,074 kg). A simple mass-balance suggests a net of about 7 million metric tons of CO₂ (6,944,587,674 kg) are sequestered in the SACROC northern platform.

ANALYSIS OF COMPETING CO₂ TRAPPING MECHANISMS AT SACROC NORTHERN PLATFORM

We developed two different models representing CO₂ trapping mechanisms at the SACROC northern platform, both utilizing the hydrogeologic framework, boundary conditions, and sources/sinks described above. The objective of these two simulations was to predict and compare the major trapping mechanisms, including hydrostratigraphic, residual, brine-solubility, oil-solubility, and mineralization.

The first model was designed for simulating CO₂ trapping mechanisms in a reservoir saturated with brine only. The other model was designed for simulating CO₂ trapping mechanisms in a reservoir saturated with both brine and oil. The latter model provides a relatively realistic representation of CO₂ trapping mechanisms in the SACROC field because this field is a petroleum reservoir subjected to a long history of CO₂ injection for enhanced oil recovery. We conducted all simulations during a 200-year time period from 1972 to 2172. All simulations were performed with the CMG's GEM simulator, a multi-dimensional, finite-difference, isothermal compositional simulator (Computer Modeling Group, 2008).

SACROC CO₂ Trapping Model—Brine Only

Initial conditions.—From 1954 to 1971, water was injected in a centerline pattern to increase the reservoir pressure above bubblepoint pressure (12.45 MPa) as illustrated in Dicharry and others (1973) and Langston and others (1988). As a result, when CO₂ injection began in 1972, reservoir pressure had risen above 16.55 MPa. This pressure condition is assigned as the initial average reservoir pressure (16.55 MPa) in the upscaled geocellular model with 15,470 (=17×35×26) elements shown in figure 8D. To achieve this average pressure, reservoir pressure was assigned as hydrostatic pressure from the formation top equal to 15.73 MPa to the bottom pressure equal to 17.90 MPa in the upscaled model. Langston and others (1988) reported the reservoir temperature as 54.5°C, and we used this value as an average reservoir temperature. In the model, the initial reservoir temperature was assigned using a conductive gradient with temperature at the top equal to 54.35°C and bottom equal to 59.83°C. The assigned temperatures in the model remain constant during the simulation period although there could be an occurrence of a non-isothermal effect caused by CO₂ injection and migration. We refer readers to other studies about the detailed non-isothermal effect related to CO₂ sequestration processes (Bielinski and others, 2008; Lu and Connell, 2008; André and others, 2010; Han and others, 2010b).

Boundary conditions.—Through rigorous analysis of water chemistry data, we were able to predict a possibility of local contamination of shallow groundwater caused by either surface recharge of recycled brine or leakage of CO₂-saturated brine through the Wolfcamp Shale Formation. Local brine-contamination notwithstanding, we assume that the Wolfcamp Shale Formation is a sufficient sealing unit. Some observations that justify this assumption include

- (1) The Wolfcamp Shale Formation, as thick as 150 m, was a seal for hydrocarbon in the Cisco and Canyon Groups during vast periods of geologic time (Vest, 1970; Raines and others, 2001).
- (2) Measured vertical permeability (k_z) in the Wolfcamp Shale Formation is low (<0.05 mD) enough to prevent vertical CO₂ migration according to Carey and others (2007).
- (3) X-ray diffraction analysis suggests that carbonate minerals in the Wolfcamp Shale formation appear to derive from primarily diagenetic processes and their isotope compositions show typical marine-originated $\delta^{13}\text{C}$ values (Carey and others, 2007).
- (4) CO₂ fugacity in reservoir fluids of Cisco and Canyon Groups significantly increases during the CO₂ injection period (table 1) but CO₂ fugacity does not vary in shallow groundwater above the Wolfcamp Shale Formation (table 4).

As such, we assigned a no-flow condition at the upper boundary in the 3-D upscaled geocellular model. Although both Kaszuba and others (2005), Xu and others (2005), and Busch and others (2008) indicate that the caprock can also act as a reactive component and contribute to mineralization, we think that the role of the caprock as a reactive component is not significant since the flow mechanism in the caprock is dominantly diffusion-driven. Gaus and others (2005) concluded that the mineralization due to diffusion in typical seals occurs in the lower 2 m after 3000 years. Similarly, Lu and others (2009) measured carbon isotopes from mudrock seal immediately above a natural CO₂-rich reservoir in the North Sea Miller oil field and suggested that CO₂ migrated only 12 m through mudrock seal during 70 to 80 million years. As described, the mineralization within such caprocks will be much smaller than that in the targeted reservoir formations. Therefore, treating the seals as no-flow boundaries will not significantly affect the prediction of CO₂ trapping mechanisms and capacity estimation.

Due to these reasons, the eastern, western, and northern boundaries are treated as no-flow boundaries because the Wolfcamp Shale Formation meets these boundaries; the carbonate reef complex of the Cisco and Canyon Groups is prism-shaped (Vest, 1970). The bottom boundary is also designated as a no-flow boundary because the Strawn Formation below the Cisco and Canyon Groups is also a low permeable unit (Raines, Kinder Morgan CO₂ Inc., personal communication, 2006). Finally, a hydrostatically constant pressure condition known as the “Dirichlet” condition is assumed at the southern boundary of the model because this boundary is connected to the middle part of the SACROC Unit (fig. 1C).

Transport and chemistry input data.—Relative permeability curves of supercritical-phase CO₂ ($k_r^{CO_2}$) and brine (k_r^{br}) in the 3-D geocellular model were developed by extrapolating $k_r^{CO_2}$ data measured by Bennion and Bachu (2005). They measured $k_r^{CO_2}$ and k_r^{br} in a 0.16 m core of low-permeability carbonate rock collected from Wabamun Lake, with experimental conditions of 41°C and 22.4 MPa. Hysteretic effects were included in the $k_r^{CO_2}$ curve using a modified Land equation (Land, 1968; Kumar and others, 2005; Han and others, 2010a).

$$k_r^{CO_2}(S_{CO_2}) = k_r^{CO_2}(S_{CO_2}) \text{ during drainage} \quad (3)$$

$$k_r^{CO_2}(S_{CO_2}) = k_r^{CO_2}(S_{CO_2}(\text{shifted})) \text{ during imbibition} \quad (4)$$

Where

$$S_{CO_2}(\text{shifted}) = \frac{S_{CO_2} - S_{gh}}{S_{gh} - S_{gh}} S_{gh} \quad (5)$$

TABLE 5

Volume fractions, surface areas, and kinetic rates assigned in the upscaled geocellular model

Mineral	Weight percent (Carey, 2007)	Modified weight percent	Volume fraction	Surface area (m ² /m ³)	Activation energy (J/mol)	Logk ₂₅ (mol/m ² s)	Model kinetic rate
Calcite	0.82	0.62	0.6063	586.72	41870	-8.80	Svensson and Dreybrodt, (1992)
Dolomite	0	0.1	0.0933	559.86	41870	-9.22	White, (2005)
Kaolinite	0.01	0.01	0.0110	6115.38	62760	-13.00	Nagy, (1995)
Anhydrite	0	0.1	0.0892	535.35	41870	-8.80	Same as calcite
Quartz	0.03	0.03	0.0303	606.87	87500	-13.90	Tester and others, (1994)
Illite	0.02	0.02	0.0193	5781.82	58620	-14.00	Knauss and Wolery, (1989)
Ankerite	0.12	0.12	0.1043	521.31	41870	-10.22	Estimated from Dolomite
Dawsonite	0	0	0	657.02	62760	-9.09	Hellevang, (2005)
Siderite	0	0	0	401.52	41870	-10.22	Estimated from Dolomite

and

$$\frac{1}{S_{gr}^{\max}} = \frac{1}{S_{grh}} - \frac{1}{S_{gh}} + 1 \quad (6)$$

S_{gh} is the value of S_{CO_2} when the shift to imbibition occurs. S_{grh} is the value of S_{gr} corresponding to S_{gh} . Adopting the Land equation requires the determination of maximum residual saturation (S_{gr}^{\max}). An empirical formulation ($S_{gr}^{\max} = 0.5473 - 0.969\phi$) determining S_{gr}^{\max} from porosity (ϕ) was proposed by Holtz (2002). Using this empirical formulation, S_{gr}^{\max} was calculated as 0.4 in this model. Capillary pressure curve for brine and supercritical-phase CO₂ was also developed by extrapolating data measured by Bennion and Bachu (2006). Here, for simplification, the same capillary pressure curve is used for both drainage and imbibition conditions, and the scaling of capillary pressure curve dependent on heterogeneous permeability field (Leverett, 1941; Durmore and Schols, 1974) is not implemented. We refer readers to Plug and Bruining (2007) and Saadatpoor and others (2010) for this specific topic in relation to geologic CO₂ sequestration. Both CO₂ density and viscosity were respectively calculated from the Peng-Robinson equation of state (Peng and Robinson, 1976) and Jossi and others (1962). CO₂ solubility was calculated using Henry's law (Li and Nghiem, 1986) adjusted for the effects of temperature (Harvey, 1996), salinity, and salting out (Bakker, 2003). Drying out effects due to brine evaporation at the vicinity of injection wells was not considered in this work since our primary objective was to identify CO₂ trapping mechanisms at a reservoir scale. We refer readers to other studies for discussion of salt precipitation effects near CO₂ injection wellbores due to drying out processes (André and others, 2007; Giorgis and others, 2007; Pruess and Müller, 2009) and studies of mutual solubility (Duan and Sun, 2003; Spycher and others, 2003). Finally, density and viscosity of the CO₂-H₂O aqueous mixtures with the effects of brine concentration were estimated using data and relationships discussed by Rowe and Chou (1970) and Kestin and others (1981), respectively.

We assigned mineralogy in the 3-D upscaled geocellular model based on X-ray diffraction analyses results (table 5) measured by Carey and others (2007) who analyzed core samples collected from Cisco and Canyon Groups. In their analyses, dolomite and anhydrite were not detected. However, previous geological studies described in Section "Geologic Descriptions" indicated that the Cisco and Canyon Groups

were highly altered by calcitization and dolomitization processes and included minor amounts of anhydrite, dolomite, sand, and shale (Bergenback and Terriere, 1953; Myers and others, 1956; Raines and others, 2001). Therefore, we modified mineralogy to include dolomite and anhydrite (table 5).

Geologic studies suggest that dawsonite specifically is considered to be a late-stage mineral deposited in natural CO₂ reservoirs (Baker and others, 1995; Moore and others, 2005). Due to this reason, the possibility of dawsonite precipitation during CO₂ sequestration processes has been studied with various experiments (Kaszuba and others, 2005; Hellevang and others, 2005; Bénézech and others, 2007). In the SACROC Unit, Carey and others (2007) previously found a single X-ray diffraction peak of dawsonite in the SACROC core and indicated the possibility of dawsonite precipitation. Therefore, in the 3-D upscaled geocellular model, dawsonite was chosen for the secondary minerals with siderite.

Since no direct measurements of BET-surface areas are available, the specific surface area ($A_m = (A \times v \times \rho_m) / (V \times M_w)$) proposed by Knauss and others (2005) was calculated using grain volume ($V: [m^3]$), grain surface area ($A: [m^2]$), molar volume ($v: [m^3/mol]$), molecular weight ($M_w: [g/mol]$), and mineral density ($\rho_m: [g/m^3]$), as detailed in table 5. To calculate V and A , the mineral grains are assumed to be spherical. An average grain radius of 0.00125 m is assumed for all minerals except clay minerals (0.000125 m) such as kaolinite and illite.

The kinetic rate law for the dissolution and precipitation of minerals is from Lasaga (1984) with a temperature-dependent rate constant derived by Arrhenius' law:

$$r_m = \text{sgn} \left(A_m k_{25} \exp \left[-\frac{E_a}{R} \left(\frac{1}{T} - \frac{1}{298.15} \right) \right] \left(1 - \frac{Q_m}{K_m} \right) \right) \quad (7)$$

Where, m is the mineral index, r is the dissolution/precipitation rate [mol/m^3s] (positive value indicates precipitation and negative value indicates dissolution), A_m is the reactive surface area [m^2/m^3], k_{25} is the kinetic rate coefficient at 25°C [mol/m^3s], E_a is the activation energy [J/mol], R is the gas constant [$8.314 J/mol K$], K_m is the equilibrium constant for mineral reaction, and finally, Q_m is the activity product. As shown in eq 7, the kinetic rate law is limited to describe the growth of secondary minerals in relation to nucleation, preferential growth, and Ostwald ripening, with which only a few studies have been previously concerned (Steefel and van Cappellen, 1990; Ozkan and Ortoleva, 2000). In addition, the kinetic rate constant is often expressed as the sum of three mechanisms such as neutral, acid, and base mechanisms (Lasaga and others, 1994; Palandri and Kharaka, 2004). Among these three mechanisms, only the neutral mechanism is considered here for simplicity. The kinetic rate coefficients and activation energies of different minerals assigned in the 3-D upscaled geocellular model are summarized in table 5. Some kinetic data are taken directly from the scientific literature and others are set to minerals with known kinetic properties.

Thermodynamic parameters, including equilibrium constants, were chosen from the SOLMINEQ.88 and PHREEQC databases (Kharaka and others, 1989; Parkhurst and Appelo, 1999). Particularly, the equilibrium constant of ankerite, which is a solid-solution between siderite and dolomite, varies with its composition. In a natural system, a binary solid-solution, $Ca(Fe_xMg_{1-x})(CO_3)_2$, where $Mg^{2+} \gg Fe^{2+}$ has been observed (Mozley and Hoernle, 1990), but the end-member ankerite, $CaFe(CO_3)_2$, has not (Chai and Navrotsky, 1996). Therefore, the composition of ankerite is assumed to be $CaFe_{0.25}Mg_{0.75}(CO_3)_2$ and its equilibrium constant is calculated from a regular solid-solution approach (Appelo and Postma, 1993) using free energy data from Wood and Garrels (1992). The detailed calculation of ankerite's equilibrium constant is described in Han (ms, 2008).

TABLE 6

Description of primary and secondary species and their initial concentrations

Primary species	Concentration (mol/l)		Secondary species
H ⁺	3.981E-7 (pH=6.4)		CO ₃ ²⁻
K ⁺	3.981E-7	Estimated	NaCl(aq)
Na ⁺	1.094E0		NaCO ₃ ⁻
Ca ²⁺	1.314E-1		NaHCO ₃ (aq)
Mg ²⁺	5.700E-2		CaCO ₃ (aq)
SiO ₂ (aq)	2.345E-3	Estimated	CaHCO ₃ ⁺
Al ³⁺	2.318E-11	Estimated	MgCO ₃ (aq)
Fe ²⁺	8.850E-4		MgHCO ₃ ⁺
Cl ⁻	1.391E0		Al(OH) ₄ ⁻
HCO ₃ ⁻	5.300E-2		Al(OH) ₃ (aq)
SO ₄ ²⁻	4.050E-2		Al(OH) ₂ ⁺
			Al(OH) ²⁺
			FeCl ₄ ²⁻
			FeCl ⁺
			Fe(OH) ₂
			Fe(OH) ⁺
			H ₄ SiO ₄ (aq)

For the activity coefficient calculation, the B-dot model (Helgeson, 1969) was implemented in this study because this model is relatively easy to incorporate new species and estimate activity coefficients under high temperature conditions. However, the Pitzer model (Pitzer, 1987) can accurately describe the behavior of electrolyte solutions especially at high ionic strength fluid (Monnin, 1989; Lichtner and Felmy, 2003; Zhang and others, 2006), and furthermore, the Pitzer's ion interaction parameters for various aqueous species are becoming more available (Harvie and others, 1984; Felmy and others, 1994; Azaroual and others, 1997; Accornero and Marini, 2009). In CO₂ sequestration processes, the reservoir fluids into which supercritical-phase CO₂ is injected typically have high ionic strengths. Therefore, the application of the Pitzer model can improve the prediction of activity coefficients compared to the B-dot model implemented in this work. Recently, Gaus (2010) discussed the essentials of the Pitzer model in a CO₂ sequestration problem. From the discussion in Gaus (2010), the application of the Pitzer model coupling into reactive transport simulator, TOUGHREACT, is currently ongoing (Zhang and others, 2006), and the development of the complete database for the Pitzer ion interaction parameters is going to be an essential task. Finally, we acquired the initial concentration of brine chemistry (table 6) in the upscaled geocellular model by batch geochemical modeling with the input of average values of brine water chemistry data (table 1) and mineralogy (table 5).

Assignment of CO₂ injection and production wells.—More than 300 wells have been used for CO₂ injection and production over the last 35 years in the SACROC northern platform. Because the sizes of grid elements in the upscaled geocellular model are larger than the distance between individual wells in the actual field, we were forced to lump groups of wells within each grid element. Each was assigned as an inverted 5-spot pattern, and as such we could not assign the actual number of injection and production wells. Consequently, we implemented 23 pumping (*P*) wells and 22 injection (*I*) wells in the 3-D upscaled model (fig. 8D). In addition, both injection and production

wells are partially penetrated with the intervals of 10 to 20 m, approximately 40 m above from the bottom of the model.

We simulated CO₂ injection and production in the field for a 30-year period, from 1972 to 2002. During this field-operation period, a net of about 6.9 million metric tons of CO₂ (6,944,587,674 kg) has been sequestered in the SACROC northern platform (see the discussion in “SOURCES AND SINKS: ACTUAL CO₂ INJECTION AND PRODUCTION HISTORIES”). Nevertheless, in the 3-D upscaled geocellular model, the exact field injection and production history do not match because of issues associated with the scale of the upscaled grid. Rather, only net storage at the end of injection period was matched. In the upscaled model, the CO₂ net storage was about 6.7 million metric tons (6,745,407,000 kg). Consequently, the relative error of CO₂ net storage between the actual field and the model is 2.9 percent.

Results: Spatial distribution of hydrostratigraphic (mobile)- and residual-trapped CO₂.—Figures 10A and 10B respectively show the spatial distribution of supercritical-phase CO₂ and the associated $k_r^{CO_2}$ values, 100 years after CO₂ injection starts (year 2072). Due to the difficulty of showing three-dimensional distributions, two-dimensional cross-sectional views/slices are presented instead. By comparing the spatial distribution between CO₂ saturation (fig. 10A) and associated $k_r^{CO_2}$ values (fig. 10B), it is possible to distinguish the location of free (mobile) CO₂ and residual (immobile) CO₂. By definition, supercritical-phase CO₂ becomes mobile when the $k_r^{CO_2}$ value is greater than zero. In reverse, the supercritical-phase CO₂ becomes immobile, and its $k_r^{CO_2}$ value is equal to zero. In figure 10A, CO₂ saturation is greater than zero within the CO₂ plumes. However, figure 10B shows that although certain grid-blocks have CO₂ saturations greater than zero, they have a zero value for $k_r^{CO_2}$. These grid-blocks indicate where CO₂ is trapped as a residual form.

According to Juanes and others (2006), mobile CO₂ is located at the front of the CO₂ plume, while residual-trapped CO₂ is located at the tail of the CO₂ plume. Similarly, in this simulation, $k_r^{CO_2}$ values were greater than zero at the front of the CO₂ plume, indicating the presence of mobile CO₂. However, $k_r^{CO_2}$ values were zero at the tail of the CO₂ plume although values of CO₂ saturations were not zero, indicating that supercritical-phase CO₂ was stored in a residual form at the tail of the CO₂ plume. Finally, the distribution of aqueous-phase CO₂ imitates the distribution patterns of supercritical-phase CO₂, but with a wider extent (fig. 10C).

Results: Spatial and temporal distribution of aqueous species and minerals.—For most minerals (especially silicate minerals), two hundred years is an insufficient time to reach equilibrium with reservoir fluids. Even after 200 years, all minerals in the simulation results are still dissolving or precipitating. Generally, mineral changes initiate as the dissolution of CO₂ lowers the pH of reservoir brine, which has also been observed in previous laboratory and field experiments (Bowker and Shuler, 1991; Klusman, 2003; Kaszuba and others, 2005; Kharaka and others, 2006). Decreasing pH subsequently induces changes in aqueous concentrations and minerals. In this simulation, initial pH of the reservoir fluid was 6.4 at year 1972 and decreased to approximately 4.5 at year 2072 after 100 years (fig. 11A). The pH does not decrease below 4.5 because the carbonate rock acts as a buffer. Specifically, the simulated pH (fig. 11A) in the brine-only model was decreased more than the observed pH from the SACROC oil field (table 1). Although various processes and uncertainties among model parameters could result in the discrepancy of model predicted pH, we presume that one of the main causes would be the presence of oil in the field.

Calcite, the major mineral in the SACROC Unit, predominantly dissolves during a 200-year simulation. Both anhydrite and dolomite are the major minerals precipitated in this same period. Dawsonite and ankerite are also precipitated but in minor

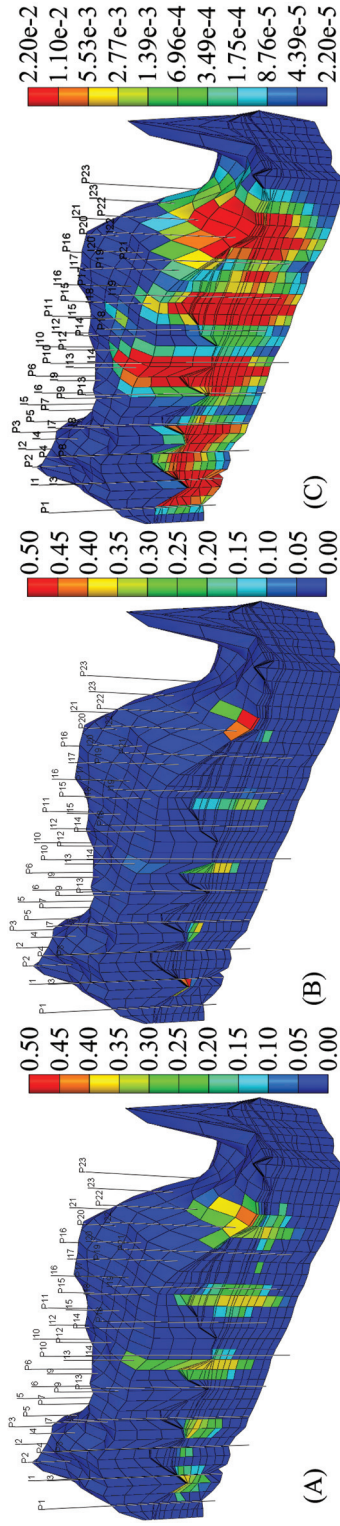


Fig. 10. Two-dimensional cross-section view at year 2072 (100 years after CO₂ injection starts): (A) saturation of supercritical-phase CO₂ with the linear scale, (B) relative permeability (k_{r,CO_2}) of supercritical-phase CO₂ with the linear scale, and (C) mole fraction of aqueous-phase CO₂ with the logarithmic scale.

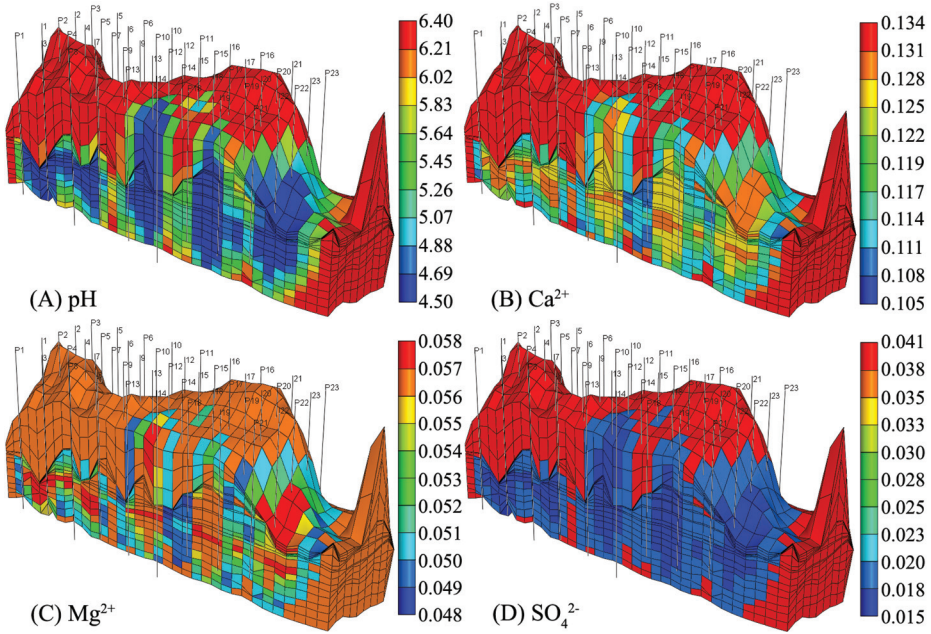
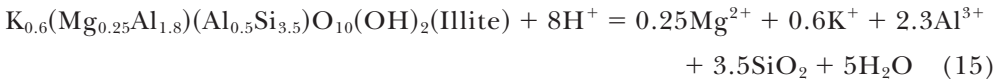
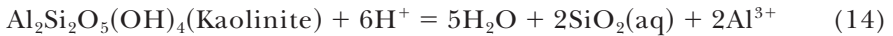
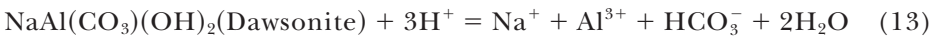
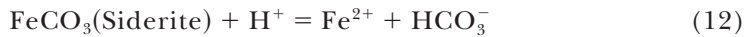
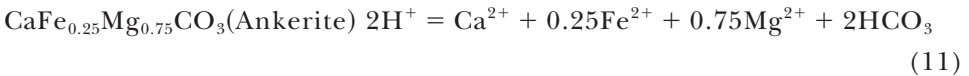
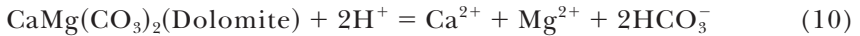
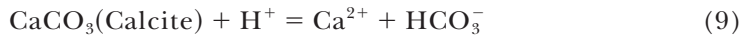
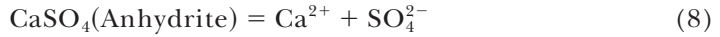


Fig. 11. Two-dimensional cross-section view at year 2072 (100 years after CO₂ injection starts): (A) pH, molalities of (B) Ca²⁺, (C) Mg²⁺, and (D) SO₄²⁻.

amounts. In addition to the carbonate minerals, kaolinite and illite respectively precipitated and dissolved. The associated mineral reactions in this model are:



Mineral precipitation and dissolution patterns are closely related to spatially varying aqueous species. Figure 11B shows the spatial distribution of Ca²⁺ ions. Calcite dissolution (eq 9 and fig. 12A) supplies Ca²⁺ ions to the reservoir brine and triggers the precipitation of dolomite (eq 10 and fig. 12B), anhydrite (eq 8 and fig. 12C), and ankerite (eq 11 and fig. 12D). Especially, CO₂ injection induces the dolomitization process with concurrent calcite dissolution. Previous laboratory studies suggested that elevated temperature, exceeding 60°C, initiates precipitation of dolomite (Uzdowski,

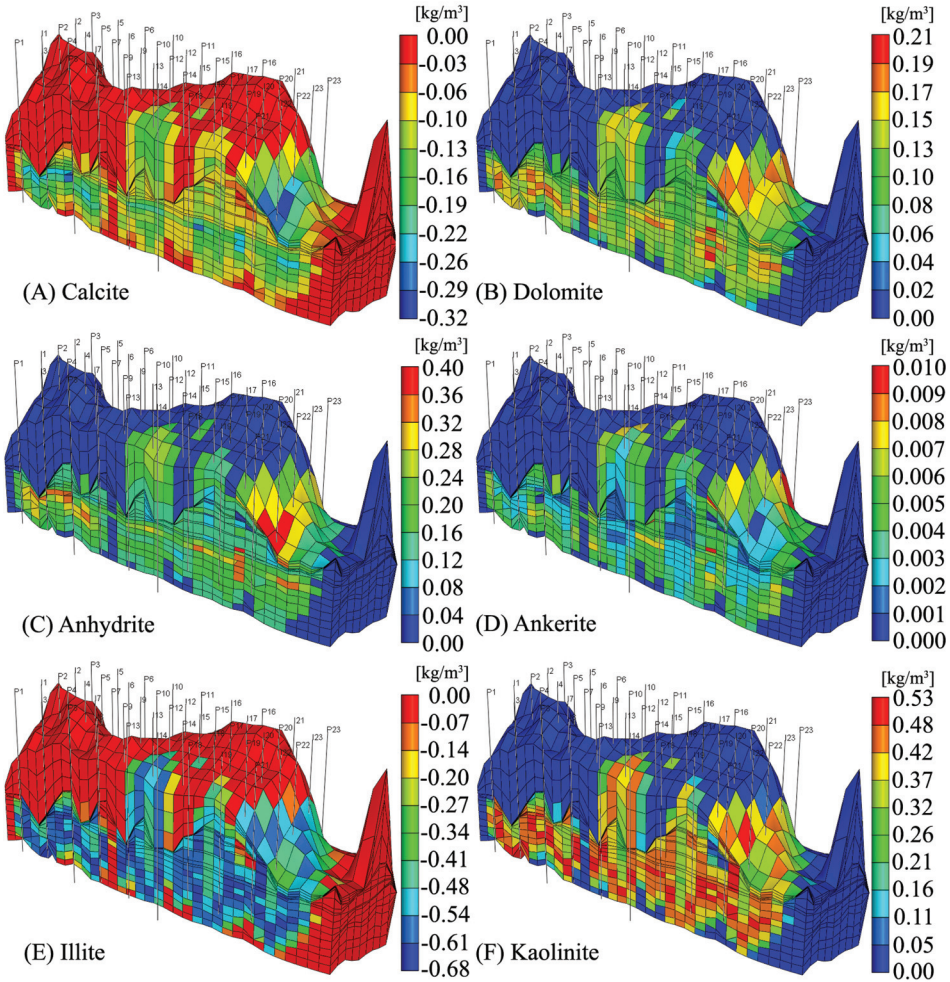


Fig. 12. Two-dimensional cross-section view of minerals (kg/m^3) at year 2072 (100 years after CO₂ injection starts): (A) calcite, (B) dolomite, (C) anhydrite, (D) ankerite, (E) illite, and (F) kaolinite.

1994) although dolomite generally does not precipitate at surface temperature. Similarly, the model predicts that subsurface reservoir temperature is close to 60°C in the SACROC Unit and a high Mg²⁺ concentration in brine fluid initiates dolomite precipitation.

Figure 11C shows the spatial distribution of Mg²⁺ ions, which are consumed during the precipitation of dolomite (fig. 12B) and ankerite (fig. 12D), and concurrently, supplied from the dissolution of illite (fig. 12E). Mg²⁺ concentration in brine fluid was initially 0.057 molality and was depleted to approximately 0.050 molality (fig. 11C) after 100 years (year 2072), suggesting that the Mg²⁺ ion consumption for dolomite and ankerite precipitations is greater than Mg²⁺ ions supply from illite dissolution. In addition to illite, other Mg-bearing aluminosilicates such as montmorillonite and saponite occur naturally. Although these two minerals were not implemented in this simulation, the presence of these minerals in a natural system could affect both Mg²⁺ and Al³⁺ concentration. Finally, calcite dissolution and high SO₄²⁻ concentration in

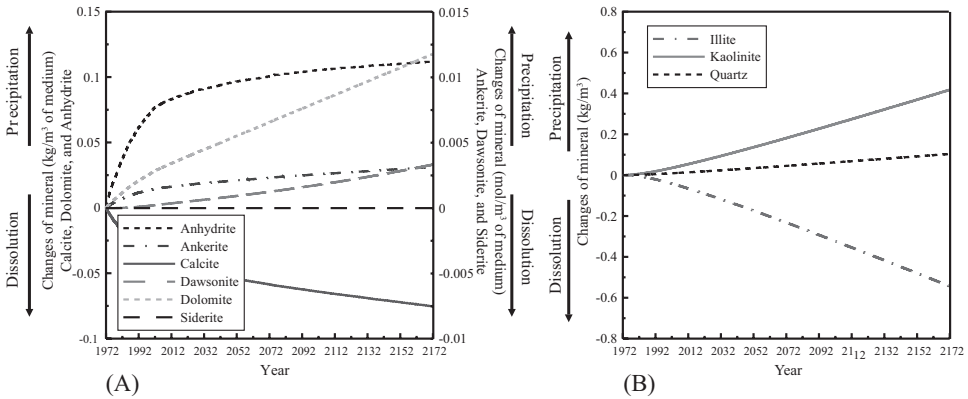


Fig. 13. Temporal evolution of net changes of minerals per the total model volume (kg per m³): (A) carbonate minerals and (B) silicate and clay minerals.

reservoir brine induces anhydrite precipitation (fig. 12C). Due to anhydrite precipitation, SO₄²⁻ concentration in the brine fluid decreased from an initial 0.04 molality to 0.018 molality after 100 years (fig. 11D).

Reactions involving aluminosilicate minerals have been observed experimentally by Bertier and others (2006). In this SACROC simulation, illite and kaolinite respectively dissolved and precipitated (figs. 12E and 12F). Although kinetic rates of aluminosilicate minerals are slow, the chemical reactions of such aluminosilicate minerals can change the concentration of Al³⁺ ions in brine and cause dawsonite to precipitate (Xu and others, 2004; Hellevang and others, 2005; Audigane and others, 2007). In this simulation, Al³⁺ is supplied from illite dissolution and consumed for the precipitation of kaolinite and dawsonite. Through the simulation period, Al³⁺ ions increases from 10⁻¹¹ to 10⁻⁷ molality due to the dissolution of illite mineral. Consequently, the change in Al³⁺ ion concentration causes precipitation of a small amount of dawsonite after 100 years. Again, the presence of other aluminosilicate minerals in a natural system could affect this process.

In addition to the spatial distribution of minerals, the temporal evolutions of net changes of minerals per the total model volume (kg per m³) are predicted during the 200-year simulation period and plotted in figures 13A and 13B. Over a 200 year period, approximately 0.12 kg per m³ of dolomite, 0.11 kg per m³ of anhydrite, 0.003 kg per m³ of ankerite, 0.003 kg per m³ of dawsonite are precipitated, and about 0.076 kg per m³ of calcite is dissolved (fig. 13A). In addition to carbonate minerals, 0.43 kg per m³ of kaolinite, 0.11 kg per m³ of quartz are precipitated, and about 0.56 kg per m³ of illite is dissolved (fig. 13B).

The mineral changes of simulated dissolution and precipitation cause changes in porosity. The altered porosity field is shown in figure 14A, indicating the net reduction ($\Delta\phi = \phi_{\text{initial}} - \phi_{\text{current}}$) of porosity due to CO₂ injection. After 100 years, mineral precipitation due to CO₂ sequestration causes the reduction of porosity by approximately 7.5e-5. The corresponding changes of permeability are calculated from the Kozeny-Carman model:

$$\frac{k_{\text{current}}}{k_{\text{initial}}} = \left(\frac{\phi_{\text{current}}}{\phi_{\text{initial}}}\right)^3 \left(\frac{1 - \phi_{\text{initial}}}{1 - \phi_{\text{current}}}\right)^2 \quad (16)$$

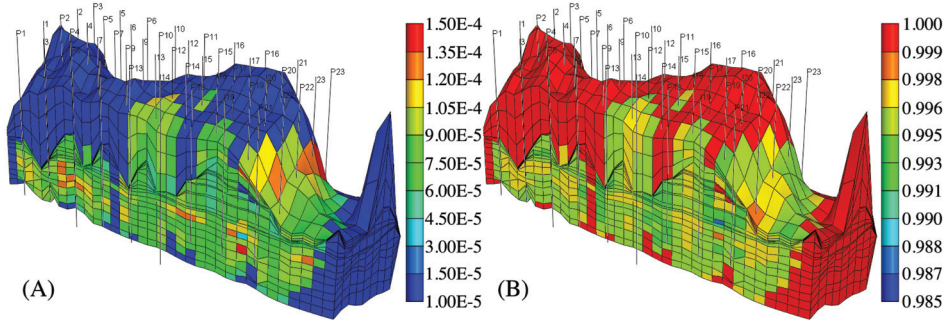


Fig. 14. Changes of porosity ($\Delta\phi = \phi_{initial} - \phi_{current}$) and permeability ($k_{current}/k_{initial}$) at year 2072 (100 years after CO₂ injection starts): (A) porosity and (B) permeability.

where ϕ is the porosity, k is the permeability (m²). The altered permeability field ($k_{current}/k_{initial}$) is shown in figure 14B. The corresponding permeability reduction was about 0.993.

Results: Quantification of CO₂ trapping mechanisms.—Figure 15A summarizes the CO₂ mass stored in different forms, with CO₂ trapping mechanisms detailed in injection and post-injection periods. During the injection period (1972-2002), 6.7 million metric tons of CO₂ are sequestered into the Cisco and Canyon Groups of the 3-D upscaled geocellular model. In this period, the CO₂ saturation gradually increases near the injection wells. At the same time, the CO₂ plume migrates either vertically or horizontally through preferential flow paths due to the injection-induced pressure. Specifically, the amount of mobile CO₂ increases up to 5.0 million metric tons without increasing immobile CO₂ until the end of the injection period, suggesting that a drainage process [CO₂ (=the non-wetting phase) displaces brine (=the wetting phase)] occurs. In addition, CO₂ injection increases reservoir pressure, leading to the increased CO₂ dissolution in brine. As a result, the mass of solubility-trapped CO₂ sharply increases up to 1.7 million metric tons at the end of the injection period.

After CO₂ injection ends (2002-2172; post injection period), the CO₂ plume starts to migrate upward due to the buoyant force associated with the density contrast between reservoir brine and CO₂. While the CO₂ plume migrates vertically, some CO₂ becomes trapped as a residual form at the tail of the CO₂ plume where imbibition (brine displaces CO₂) occurs. Due to this process, the amount of residual-trapped CO₂ increases dramatically immediately after CO₂ injection stops, and consequently, the amount of mobile CO₂ decreases (fig. 15A). Simulation results suggest that the vertical CO₂ migration after injection stops is the critical factor governing the residual CO₂ trapping mechanism. After 200 years of CO₂ injection, the mass of mobile CO₂ and immobile CO₂ becomes 1.5 million and 2.8 million metric tons, respectively. Finally, the mass of solubility-trapped CO₂ continues to increase to 2.3 million metric tons, but at a slower rate because injection-induced CO₂ partial pressure decreases almost immediately after CO₂ injection ceases. Relatively small amounts (0.17 million metric tons of CO₂) of minerals precipitate after 200 years.

As shown, previous researchers concurred that the most effective short-term storage mechanism is residual CO₂ trapping, and its sensitivity is strongly dependent on S_{gr}^{max} in the Land hysteresis equation shown as eq 6 (Kumar and others, 2005; Juanes and others, 2006; Doughty, 2007). However, until now, only one laboratory dataset (Suekane and others, 2008) predicting S_{gr}^{max} in the supercritical CO₂/brine system has been available. Due to this reason, many researchers rely on one fitting equation developed with data from gas reservoirs (Holtz, 2002). Therefore, we performed

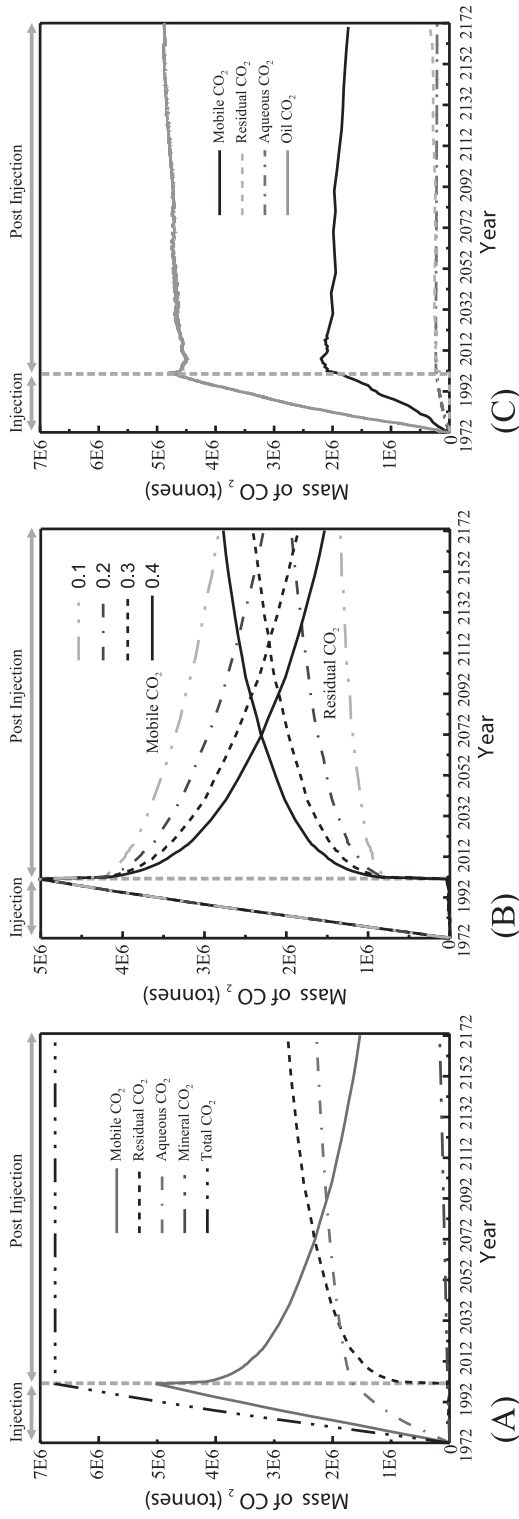


Fig. 15. (A) CO₂ trapping mechanisms in brine-only model as a function of time, (B) sensitivity studies of mobile and residual-trapped CO₂ with S_{gr}^{max} in brine-only model, and (C) CO₂ trapping mechanisms in brine + oil model as a function of time.

TABLE 7

Initial oil composition (Dicharry and others, 1973) in the upscaled geocellular model

Oil Composition	Mol	Molecular Weight
CO ₂	0.0032	44.01
N ₂	0.0083	28.01
C1(Methane)	0.2865	16.04
C2(Ethane)	0.1129	30.07
C3(Propane)	0.1239	44.10
I-C4(I-Butane)	0.0136	58.12
N-C4(N-Butane)	0.0646	58.12
I-C5(I-Pentane)	0.0198	72.15
N-C5(N-Pentane)	0.0251	72.15
FC6(Hexane)	0.0406	86.00
C7+(Heptanes plus)	0.3015	275.00

sensitivity studies of CO₂ trapping mechanisms with S_{gr}^{max} . Simulation results predicted that the amount of residual-trapped CO₂ increases with larger S_{gr}^{max} (fig. 15B). For example, residually trapped CO₂ with 0.1 S_{gr}^{max} was 1.35 million metric tons after 200 years and with 0.4 S_{gr}^{max} was 2.78 million metric tons. Results suggest that the predicted amount of residually trapped CO₂ can be doubled with the choice of S_{gr}^{max} .

SACROC CO₂ Trapping Model—Oil and Brine

Initial and boundary conditions.—The initial conditions for pressure and temperature distribution and boundary conditions are the same as those described in the previous section “SACROC CO₂ Trapping Model—Brine Only”. However, the initial condition for fluid saturation is different from that of the brine-only model. The reservoir is assumed to be saturated with both water (0.28) and oil (0.72), following reservoir characterization details provided by Vest (1970). The oil phase is regarded as a mixture of 11 different gas components. The initial oil composition used is from Dicharry and others (1973), summarized in table 7.

Transport input data and well assignment.—Oil densities are calculated from the Peng-Robinson equation of state (Peng and Robinson, 1976) and Oil viscosity is estimated from Jossi and others (1962). CO₂ solubility in oil is predicted from flash calculations, which are decoupled from the transport equation and solved using the Quasi Newton Successive Substitution (Nghiem, 1983). The $k_r^{CO_2}$ curve and its hysteretic effect is the same as those in brine-only model. The k_r^{oil} curve is developed after extrapolating data from the SACROC core measured at 50°C and 1.4 MPa (Rohan and Haggerty, 1996). Finally, the feature of well assignments and performance period were the same as those described in the previous section “Assignment of CO₂ injection and production wells”.

Results: Quantification of CO₂ trapping mechanisms.—Figure 15C shows simulation results describing the temporal evolution of the CO₂ mass sequestered in the SACROC model saturated with both brine and oil. Specifically, the slope of oil-CO₂ curve is steep during the period between 1972 to 2002. Significant amounts of CO₂ (about 4.5 million metric tons) dissolved into oil during this period. Compared to CO₂ dissolved in oil, only a small amount of CO₂ (about 0.2 million metric tons) dissolves in the brine in the same period. The difference of CO₂ dissolution in both oil and brine is caused

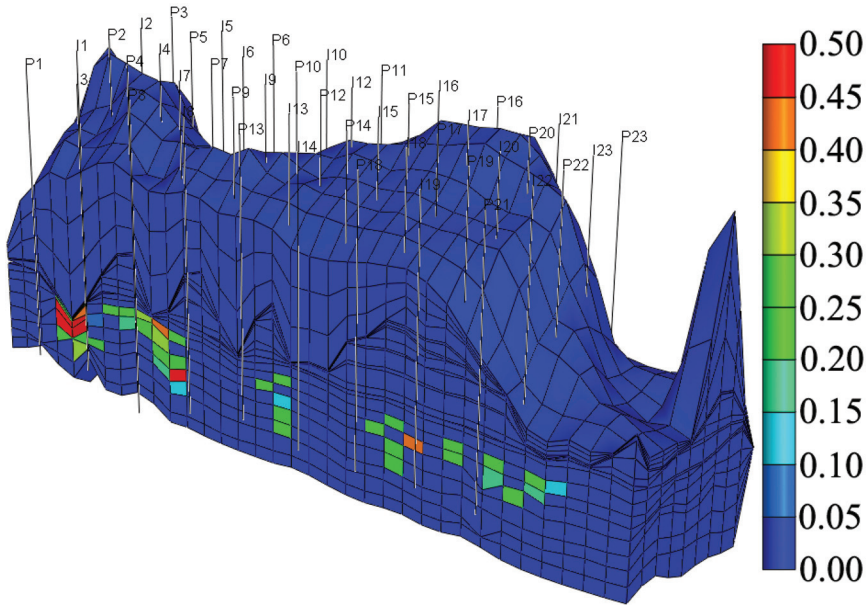


Fig. 16. Two-dimensional cross-section view of saturation of supercritical-phase CO₂ in brine+oil model at year 2072 (100 years after CO₂ injection starts).

by the difference of CO₂ solubility in both fluids and initial fluid saturation. The model predictions show that the approximate CO₂ solubility was respectively 0.010~0.018 mole fraction in brine and 0.3~0.6 mole fraction in oil at this reservoir condition. That is to say, CO₂ solubility in oil was about 30~40 times greater than that in brine. Moreover, oil saturation (0.72) was greater than brine saturation (0.28) in this model indicating that more oil volume is available for CO₂ dissolution. Therefore, the oil-solubility trapping is significantly greater than the brine-solubility trapping in this model. The amount of mobile CO₂ increased up to about 2.1 million metric tons at the end of the injection year (fig. 15C). Similar to the brine-only model, no CO₂ is trapped as a residual form during the injection period (1972-2002). Overall, the dominant CO₂ trapping mechanism is oil trapping, with about 4.5 million metric tons of CO₂ dissolved in the oil during the full 200-year simulation periods. In addition, about 2.1 million metric tons of CO₂ is stored as a mobile form.

In the previous brine-only model, the amount of mobile CO₂ is dramatically decreased and the amount of residual CO₂ is suddenly increased after CO₂ injection stops (fig. 15A). However, in the brine+oil model, the relative amounts of both mobile and residual CO₂ do not change over time (fig. 15C). Further, compared to the amount of residual-trapped CO₂ in the brine-only model, residual-trapped CO₂ in the brine+oil model is significantly less (fig. 15C). To investigate the difference of the amount of residual-trapped CO₂ in both simulations, the saturations of supercritical-phase CO₂ at year 2072 were plotted and compared (figs. 10A and 16). The comparison of CO₂ plume saturation shows that CO₂ migration behavior is distinctively different in both simulations. After 100 years, supercritical-phase CO₂ in the brine-only model migrated vertically and several CO₂ plumes were able to reach the top of the Cisco and Canyon Groups (fig. 10A). The amount of residual-trapped CO₂ increased at the tail of the CO₂ plumes while supercritical-phase CO₂ plumes migrated vertically. However, in the brine+oil model, supercritical-phase CO₂ did not migrate vertically

but stayed near the injection wells with a high CO₂ saturation (fig. 16). In general, supercritical-phase CO₂ in the brine+oil model is stored as a mobile form due to its high CO₂ saturation but does not migrate vertically due to smaller density contrast between oil and supercritical-phase CO₂ and larger CO₂ solubility in oil. Therefore, mobile CO₂ in the brine+oil model behaves like residual-trapped CO₂.

To evaluate the difference of CO₂ vertical migration behavior between brine-only and brine+oil models (figs. 10A and 16), the density of CO₂, brine, and oil phases in this model were compared. Model prediction in brine+oil model shows that the densities of CO₂, oil, and brine are, respectively, about 700~800 kg/m³, 800 kg/m³, and 1100 kg/m³ at these reservoir conditions. Since oil is a dominant fluid (72% saturation), the density contrast between supercritical-phase CO₂ and oil is smaller than about 100 kg/m³, which is 3~4 times smaller than that between supercritical-phase CO₂ and brine. Since the density contrast between oil and supercritical-phase CO₂ is small, the vertical CO₂ migration is small. (In the simulations of brine+oil model, no CO₂ plume reaches the top of the Cisco and Canyon Groups after 200 years.) Consequently, the amount of residual-trapped CO₂ is not significant (less than 0.3 million metric tons) in this model (fig. 15C). In addition to the contrast of fluid densities, CO₂ mobility is reduced when three phases coexist, for example, injecting CO₂ in a brine+oil reservoir, as opposed to injecting into a reservoir with brine only. In the brine+oil model representing a three-phase environment, the vertical movement of supercritical-phase CO₂ will be relatively retarded. Furthermore, significant CO₂ solubility in the oil phase reduces the volume of supercritical-phase CO₂ in brine+oil model and reduces buoyant force. In summary, the buoyancy-driven force was lower in the brine+oil reservoir model due to less contrast in fluid densities, smaller mobility, and larger CO₂ solubility in the oil phase. Consequently, supercritical-phase CO₂ did not migrate vertically but tended to stay closer to the injection wells.

SUMMARY AND CONCLUSIONS

The main purpose of this research was to predict CO₂ trapping mechanisms in the SACROC northern platform where about 7 million metric tons of CO₂ have been injected for the purpose of enhanced oil recovery from 1972 to 2002. This model was carefully developed with a dataset that includes injection/production history data since 1948 and water chemistry data from both reservoir brine and shallow groundwater. First, a 3-D, high-resolution, geocellular model describing the detailed reservoir structure and heterogeneity was constructed. After the renormalization process for reducing the number of model elements to manageable levels to fit on a single workstation, two models evaluating CO₂ trapping mechanisms in the SACROC northern platform were developed. Initial/boundary conditions, and other parameters in this model were carefully chosen based on the results of data analyses such as groundwater chemistry and CO₂ injection/production history. The first model was designed for simulating CO₂ trapping mechanisms in a reservoir only saturated with brine. The second model was designed for simulating CO₂ trapping mechanisms in a reservoir saturated with both brine and oil. As far as we know, this is the first attempt to compare the fate and distribution of supercritical-phase CO₂ in a reservoir containing both oil and brine versus a reservoir containing brine only. Major conclusions in this work are as follows:

1. Incorporating geologic knowledge, geophysical logs, and seismic surveys provided a foundation for interpreting 3-dimensional subsurface structures. The geocellular model reveals that the Upper Canyon Group is represented as a thick, highly porous zone (fig. 6B) and the Middle/Lower Canyon Group consists of several layered porosity zones separated by low porous carbonate mud.

2. Direct application of the subsurface structure model to develop the flow and transport models is hindered due to the lack of currently available computer resources. The renormalization technique successfully upscaled the model from 9,450,623 to 15,470 elements with a preservation of the variation of heterogeneity (figs. 8A-D).
3. Modeled CO₂ fugacity of reservoir fluids in the Cisco and Canyon Groups was significantly increased during the CO₂ injection period (table 1) but it did not vary in shallow groundwater above the Wolfcamp Shale Formation (table 4), suggesting that the Wolfcamp Shale Formation typically acts as a suitable seal in the SACROC Unit. However, analysis of water chemistry also revealed that a few shallow groundwater samples underwent local contamination with reservoir brine possibly due to the downward recharge of recycled reservoir brine from the surface during enhanced oil recovery or upward leakage of CO₂-saturated brine through the Wolfcamp Shale Formation.
4. CO₂ trapping mechanisms in the brine-only model showed two distinctive periods (fig. 15A). During the injection period (1972~2002), most supercritical-phase CO₂ is stored as mobile phase. After CO₂ injection ceases, the amount of mobile CO₂ dramatically decreases and residual-trapped CO₂ consequently increases. Therefore, during the post injection period (2002~2172), both the residual trapping and solubility trapping mechanisms become dominant. In addition, the amount of residually trapped CO₂ is strongly dependent on the S_{gr}^{max} in Land Equation (fig. 15B).
5. In the reservoir model with oil (72%) and brine (28%) phases, CO₂ trapping mechanisms do not vary distinctly over time (fig. 15C). The dominant trapping mechanism is oil trapping. Most supercritical-phase CO₂ is stored as a mobile phase near the injection wells and does not migrate; behaving much like residually trapped CO₂. This occurs because of a lower contrast in fluid densities, smaller mobility, and larger CO₂ solubility in oil phase.
6. Mobile CO₂ is located at the front of the CO₂ plume where drainage is dominant (CO₂ displaces water), while residually trapped CO₂ is located at the tail of the CO₂ plume where imbibition is dominant (water displaces CO₂).
7. Injected CO₂ is stored as several different forms of minerals in the brine-only model (figs. 13A and 13B). Calcite (0.076 kg per m³), the major mineral in the SACROC Unit, predominantly dissolves after a 200-year simulation. Both anhydrite (0.11 kg per m³) and dolomite (0.12 kg per m³) are the major minerals precipitated in the same period. Dawsonite (0.003 kg per m³) and ankerite (0.003 kg per m³) are also precipitated but in minimal amounts. In addition to the carbonate minerals, kaolinite (0.43 kg per m³) and illite (0.56 kg per m³) are precipitated and dissolved, respectively.
8. The induced porosity changes due to mineralization are minor during 100 years. Mineral precipitation due to CO₂ sequestration causes the reduction of porosity by approximately 7.5e-5 after 100 years (fig. 14A). The corresponding permeability reduction was 0.993 (fig. 14B).

The results of CO₂ trapping mechanisms presented here possess some limitations associated with upscaling, including effects of grid-coarsening and averaged (“smoothed”) values of porosity and permeability. In the geocellular model, renormalization decreases the number of elements from 9,450,623 to 15,470 as shown in table 3 and, correspondingly, increases the grid size. Through the upscaling procedure, it is clear that the contrast in permeability between adjacent elements becomes smaller (figs. 8A-D), and thus, standard deviation of effective permeability decreases (table 3). Previously, only a few studies evaluated the grid coarsening effects on CO₂ trapping mechanisms and these previous studies only considered grid effects within homoge-

neous models (Solubility trapping by Doughty and Pruess, 2004; Residual CO₂ trapping by Juanes and others, 2006; mineral trapping by Audigane and others, 2007; Yamamoto and Doughty, 2009). All these studies have suggested that the grid coarsening would generate certain errors in predicting CO₂ trapping mechanisms. Although we did not include the study associated with the grid effect here, we investigated the renormalization effect on various 2-dimensional heterogeneous permeability fields and found that the sequential renormalization underestimated residual CO₂ trapping by increasing grid scale and averaging permeability. Therefore, we expected that the residual CO₂ trapping in the presented SACROC model could be underestimated. In future work, we will employ massively parallel computing using the code, PFLOTRAN (Lu and Lichtner, 2007), to predict CO₂ trapping mechanisms in the 3-D geocellular model without the need for upscaling.

Finally, the prediction of spatiotemporal CO₂ trapping mechanisms (mobile CO₂, residual CO₂, dissolved CO₂, and mineral) is one of the daunting problems because (1) the nature of CO₂ trapping is dependent on time and space, (2) individual trapping mechanisms are strongly coupled with each other, and (3) subsurface conditions and properties are altered significantly with CO₂ injection. More importantly, it is difficult to acquire field data from the targeted formations typically below 800 m and monitor their *in-situ* variations. Therefore, previous models predicting CO₂ trapping mechanisms always included certain limitations. In this study, we utilized a specific site with the detailed 3-D geologic frame model, relevant laboratory, and field data to overcome the limitation of previous studies. As a result, this study provides the first successful quantification of all significant CO₂ trapping mechanisms concurrently based on the detailed geologic model. We expect that the processes of model development are intended to serve as an exemplary or template procedure for evaluating the relative roles of different CO₂ trapping mechanisms at other geological storage sites.

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